

Thickening supercritical CO₂ at high temperatures with rod-like reverse micelles

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20 Abstract

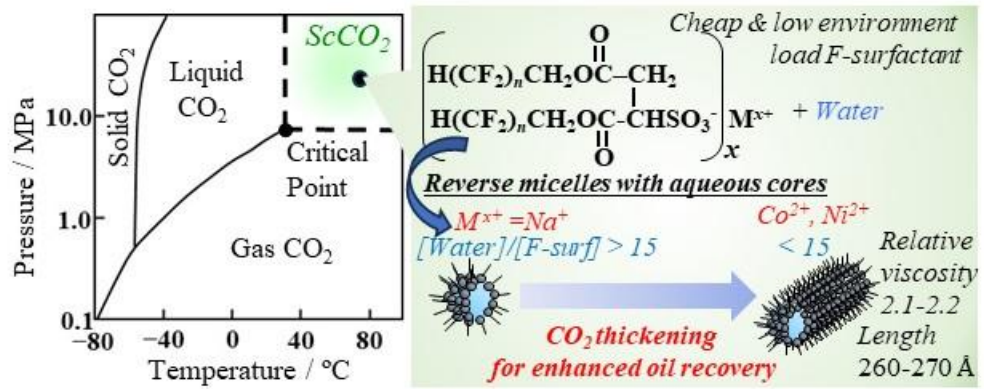
21 Earlier studies demonstrated the ability of some fluorinated surfactants to form rod-like reverse
22 micelles with thickening ability in water/supercritical CO₂ (scCO₂) mixtures at temperatures below 45 °C
23 [Langmuir 26 (2010) 83-88. *Soft Matter* 8 (2012) 7044–7055. *Colloids and Surfaces B*, 168 (2018), 201-
24 210.]. Such a viscosity enhancement of scCO₂ is known to increase sweep efficiency for oil recovery with
25 CO₂ flooding. However, temperatures of up to ~100 °C in conventional reservoirs are much higher than
26 those studied, and tend to weaken inter- and intra-molecular interactions between surfactant molecules,
27 discouraging rod-like reverse micelle formation. With the aim of designing surfactants which form rod-
28 like reverse micelles and thicken CO₂ at high temperatures, this study examined phase behavior,
29 nanostructures of reverse micelles and thickening ability of double ω-hydroperfluorocarbon-tail anionic
30 surfactants in W/scCO₂ mixtures at temperatures of 35 - 75 °C and 80 - 400 bar with different water-to-
31 surfactant molar ratios (W_0). The measured CO₂ viscosity increased by 1.9-2.2 × for double-chain
32 surfactants M(di-HCF6)_x (counterion M^{x+} = Ni²⁺ and Co²⁺) at 40 mM, over the experimental temperature
33 range. On the other hand, the shorter chain H(CF₂)₄CH₂ twin-tail surfactants M(di-HCF4)_x and Na(di-
34 HCF6) gave only 1.1-1.5 × enhancements. The maximum thickening ability of M(di-HCF6)₂ was at $W_0 =$
35 10 in the W_0 range of 5-20 75 °C and 350 bar. High pressure and temperature small-angle neutron
36 scattering (SANS) was used determine the micellar structure in these systems, and rod micelles of aspect
37 ratios of 4.5-6.5 were found. The results clearly suggest that ω-hydroperfluorohexyl-tails and divalent
38 counterions induce the formation of rod-like reverse micelles in W/CO₂ mixtures, even at high
39 temperatures commensurate with in-reservoir conditions.

40

41 Graphical abstract

42

43



44 **Highlights**

- 45 • Double ω -hydroperfluorocarbon-tail surfactants were studied in supercritical CO₂ (scCO₂)
- 46 • Surfactant induced scCO₂ thickening was observed at high temperatures commensurate with typical
- 47 reservoir conditions
- 48 • CO₂ viscosity doubled by the surfactant rod-like reverse micelles with lengths of ~ 260 Å at 75 °C
- 49 • An effective surfactant packing parameter of 1.1-1.8 is required to form rod-like reverse micelles

50

51 **Keywords**

52 Supercritical CO₂, ω -hydroperfluorocarbon, viscosity, rod-like reverse micelle, Small-Angle Neutron

53 Scattering

54

55 1. Introduction

56 Supercritical CO₂ (scCO₂) is a nonpolar solvent with attractive properties such as low cost,
57 inflammability, natural abundance, high mass transfer, and pressure/temperature-tunable solvency (CO₂
58 density) [1]. For these reasons, it has received much attention as a green solvent for industrial applications
59 like organic synthesis, dry cleaning, polymerization, extraction, nanomaterial processing, and enhanced
60 oil recovery (EOR). However, polar compounds are generally insoluble in scCO₂, limiting its use in such
61 industrial applications. For example, EOR with CO₂-flooding (CO₂-EOR), suffers a significant problem
62 that the CO₂ viscosity is notably lower than that of the crude oil to be displaced, leading to inefficient
63 volumetric sweep of the porous media [2,3]. One of the most promising approaches to increase scCO₂
64 viscosity is to generate reverse micelles in the continuous scCO₂ phase. If these micelles also contain
65 water in their polar cores, they may be termed water-in-scCO₂ microemulsions (W/CO₂ μEs) [3,4]. Such
66 multi-component self-assemblies display not only the attractive characteristics of scCO₂, but also the
67 solvation properties of bulk water, and so have potential as volatile organic compound (VOC)-free and
68 energy-efficient solvents for nano-material synthesis, enzymatic reactions, dry-cleaning, dyeing, and
69 preparation of inorganic/organic hybrid materials, amongst other potential applications [5]. For CO₂-EOR
70 processes, the reverse micelles should have a rod-like morphology leading to increased viscosity and
71 thickening of scCO₂ [3]. To broaden applications of scCO₂ it is of interest to develop highly efficient CO₂-
72 philic surfactants, which will also generate rod-like reverse micelles: this field has been actively
73 researched since the early 1990s [4].

74 Over the last three decades, there have been continued efforts developing CO₂-philic hydrocarbon
75 surfactants for W/CO₂ μE for economic and environmental reasons [4-8]. In the early 1990s, CO₂-philic
76 materials were explored in commercially available polymers, surfactants, and other oleo-philic substances.
77 However, these were mostly insoluble in scCO₂ and therefore inactive for modifying the properties of
78 scCO₂ [4]. Aerosol-OT (sodium bis-(2-ethyl-1-hexyl) sulfosuccinate, AOT), widely known as a special
79 surfactant able to stabilize effectively and efficiently water-in-oil (W/O) microemulsions [9], is also
80 insoluble in scCO₂ and hence does not stabilize W/CO₂ μEs [4]. Initial investigations clarified that

81 conventional surfactant-design theory cannot be applied to W/CO₂ systems, and that the concept “CO₂-
82 philicity” is not equivalent to oleo-philicity. Therefore, development of CO₂-philic surfactants has forced
83 new directions and paradigms in the field of surfactant molecular-design. Based on new design principles,
84 tailor-made surfactants for stabilization of W/CO₂ μEs and rod-like reverse micelles in scCO₂ have been
85 introduced [3].

86 In the earlier studies, certain fluorinated surfactants, including perfluoropolyethers (PFPFs) and
87 fluorinated AOT analogues, were reported to dissolve in scCO₂ and to reduce W/CO₂ interfacial tension,
88 hence implying feasibility for generating W/CO₂ μEs and rod-like reverse micelles [10-13]. This
89 compatibility has been explained in terms of lower surfactant interfacial packing densities and weaker
90 attractive inter-micellar interactions of FCs, which are believed to be beneficial for stabilization of W/CO₂
91 μEs compared to HCs [10-15]. The water-solubilizing power of these surfactants in CO₂ is often discussed
92 in terms of the water-to-surfactant molar ratio W_0 ($=[\text{water}]/[\text{surfactant}]$). Hereafter, the maximum W_0
93 attainable in a single-phase W/CO₂ μE, namely W_0^{max} , a measure of the solubilizing power of a given
94 surfactant.

95 With the aim of optimizing CO₂-philic surfactant structure, a range of custom-made double-tail
96 FC AOT analogues were examined [16-20]. The most efficient surfactant from this group was found to
97 be 4FG(EO)₂ which, despite having the shortest FC (perfluorobutyl) tails, could stabilize globular W/CO₂
98 μEs with $W_0^{\text{max}} = 80$ at 75°C [16]. Considering that FC tails are CO₂-philic and longer FC-tail surfactants
99 generally show higher W_0^{max} [16-20], the fact that this high stability occurs with the shortest chain FC
100 4FG(EO)₂ is at first sight surprising. In further studies, the minimum fluorine content necessary to render
101 a surfactant CO₂-philic was examined [21,22], revealing that at least two perfluorethyl groups (CF₃CF₂-)
102 were required to stabilize W/CO₂ μEs. In addition, double-FC-tail phosphate surfactants were found to be
103 efficient μE stabilizers, the most favorable case stabilizing W_0 up to 45 [23,24]. Through these
104 investigations, the effects of FC-tail chemical structure on W/CO₂ μEs stabilization and solubilizing
105 power were revealed, to identify the most efficient FC moieties.

106 An interesting class of twin-tailed hybrid surfactants, with a separate HC and FC chain have also
107 been evaluated for W/CO₂ μEs [25-29]. For example, sodium 1-pentadecafluoroheptyl-1-octanesulfate
108 (F7H7, (C₇H₁₅)(C₇F₁₅)CHOSO₃Na) gave a high solubilizing power $W_0^{\max} = 35$ [25]. On the other hand,
109 F7H7 analogues with different FC and HC chain lengths, M-F m H n (Counter ions M= Li, Na, and K,
110 perfluorocarbon length $m = 7$ and 8), successfully stabilized W/CO₂ μEs, but with smaller W_0^{\max} values
111 than for F7H7 [3,26,27]. A notable finding with this M-F7H n series was formation of rod-like reverse
112 micelles with M=Na⁺, but rather ellipsoidal or spherical with M=Li⁺, K⁺ or Rb⁺. The length and aspect
113 ratio (rod length/diameter) of Na-F7H n rod-like reverse micelles reached 525 Å and 10.5 respectively at
114 a surfactant concentration of 4.4 wt% (75 mM), $W_0 = 12.5$, at a pressure of 400 bar and temperature of 40
115 °C [3,26,27]: based on the Huggins equation relative viscosities (the ratio of micellar solution viscosity to
116 pure CO₂ viscosity) of ~2 were estimated [30,31]. Such rod-like reverse micelles with high aspect ratios
117 were expected to thicken dense CO₂, as would be required for EOR applications [3].

118 Recently, using another series of hybrid surfactants, sodium 1-oxo-1-[4-
119 (perfluoroalkyl)phenyl]alkane-2-sulfonates, FC m -HC n (FC length $m = 4, 6$, HC length $n = 2, 4, 5, 6$ and
120 8), the effects of FC and HC chain length were examined on phase stability and self-assembly structure
121 with W/CO₂ μEs at 45 °C and 350 bar [17,28,29]. The water solubilization per F-atom is another
122 interesting design concept for ranking new CO₂-philic surfactants. For these hybrid surfactants, the
123 optimal HC-tail and FC-tail lengths were found to be $n = 4$ and $m = 6$ respectively (i.e. FC6-HC4), which
124 stabilized W/CO₂ μEs with $W_0^{\max} = 80$, and a solubilizing power per F-atom of 6.2. These values are equal
125 to the highest performance and effectiveness reported in any W/CO₂ system studied so far [3-29]. The
126 structures of these FC6-HC n reverse micelles at $W_0 = 20$ (D₂O) were determined by high pressure-small
127 angle neutron scattering (HP-SANS) [28] (surfactant concentration of 17 mM, 45 °C and 350 bar).
128 Micellar shape transitions were observed on increasing HC-tail length only (ellipsoid for $n = 4$ → cylinder
129 for $n = 5$ and 6 → sphere for $n = 8$), and the aspect ratio reached a maximum of 6.3 with HC-tails $n = 6$.
130 For a surfactant concentration 35 mM, the aqueous (D₂O) rod-shaped reverse micellar core length and

131 aspect ratio for FC6-HC5 were estimated to be ~ 880 Å and 36, respectively [29]. These micellar
132 dimensions were used to estimate an intrinsic viscosity $[\eta] = 30.9$ and a specific viscosity $\eta_{sp} = 2.07$ [29].

133 Hence, the literature indicates that FC surfactants are CO₂-philic, and hence are promising as
134 stabilizers for W/CO₂ μ Es. However, FC surfactants, especially with $> C7$ like perfluorooctanoic acid
135 (PFOA) or perfluorooctane sulfonic acid (PFOS), have significant disadvantages: they are high cost, not
136 biocompatible and are environmental pollutants [32,33]. Therefore, there is quest to find alternative CO₂-
137 philic surfactants which avoid these problems. For example, ω -hydroperfluorocarbons like HCF₂-(CF₂)_n-,
138 possessing a dipole moment at the terminal HCF₂-tip: the precursor alcohol needed to synthesize
139 surfactants of this kind, H(CF₂)₆CH₂OH is known to be cheaper (90 dollar / 100g) compared to the more
140 highly fluorinated F(CF₂)₆CH₂OH (440 dollar / 100g). Furthermore, the H-terminated materials safer and
141 more environmentally acceptable due to the weaker hydrophobicity and better degradability compared
142 with F-terminated analogues [32]. Hence, there are benefits in using ω -hydroperfluorocarbons for CO₂-
143 philic surfactant tails [34-39].

144 Earlier investigations [34-39] found that a class of AOT analogues with ω -hydroperfluorocarbon
145 tails (e.g. sodium bis(1*H*,1*H*,5*H*-octafluoropentyl)-2-sulfosuccinate, Na(di-HCF₄)) stabilize W/CO₂ μ Es
146 up to $W_0 \leq 30$. The effect of the surfactant counter ion was also examined using a series of M(di-HCF₄)_x
147 analogues (counterion M = Na⁺ with $x = 1$, Co²⁺ and $x = 2$, and Ni²⁺ and $x = 2$). For these surfactants HP-
148 SANS was used to investigate micellar/microemulsion structure [38,39]. The regular sodium form, Na(di-
149 HCF₄) gave rise to spherical reverse micelles, leading to a modest increase in CO₂ viscosity of 10% even
150 at a surfactant concentration of 10 wt%. In contrast, the Co(di-HCF₄)₂ and Ni(di-HCF₄)₂ surfactants, at
151 50 mM $W_0 = 10$ at 25 °C and 400 bar, generated rod-like reverse micelles: length 300 Å with Co(di-
152 HCF₄)₂ and 700 Å for Ni(di-HCF₄)₂. Because they behave as anisotropic particles these rod-shaped
153 micelles lead to more significant CO₂ viscosity enhancements of 20-90 % at 6-10 wt% [39]. Thus,
154 employing divalent transition metal ions as counterions for CO₂-philic surfactants seems to be an effective
155 approach to addressing the CO₂ viscosity problem. The counterion effect probably originates from a

156 decrease in critical packing parameter (CPP) due to an increase in hydrophilic group area/volume induced
157 by large counter ions [39].

158 All of the rod-like reverse micelles introduced above would be very promising as CO₂-thickeners,
159 however, the temperatures are low (≤ 45 °C) compared with typical reservoir conditions (e.g. ~ 100 °C)
160 [40]. The all-important rod-like micelle formation are likely a result of interactions which are expected to
161 weaken with temperature. Therefore, to explore potential practical uses in CO₂-EOR, detailed
162 investigations at temperatures close to reservoir conditions are required.

163 With the aim of clarifying the performance of double ω -hydroperfluorocarbon-tail surfactants as
164 CO₂-thickeners, this study has examined phase behavior, viscosities, reverse micelle structures and
165 molecular properties (i.e. CPP and area per molecule) of M(di-CFn)_x and M(di-HCFn)_x in
166 water/supercritical CO₂ mixtures over 35-75 °C. The surfactants M(di-HCFn)_x have different counterions
167 (Na⁺, Mg²⁺, and Ni²⁺) and double FC tails of only low F-content (CF₃CF₂CH₂CH₂CH₂-, di-CF₂ series) or
168 ω -hydroperfluorocarbon-tail (H(CF₂)₄CH₂- (di-HCF₄ series) or H(CF₂)₆CH₂- (di-HCF₆ series). The
169 findings described here suggest new directions and strategies for developing CO₂-philic surfactants for
170 generating rod-like reverse micelles and CO₂ thickeners.

171

172 2. Experimental Section

173 2.1. Materials

174 The family of low fluorine-content surfactants studied here are Nickel 1,5-
175 bis[(1H,1H,2H,2H,3H,3H-pentafluoropentyl)oxy]-1,5-dioxobutane-2-sulfonate (Ni(di-CF₂)₂), Cobalt
176 1,5-bis[(1H,1H,2H,2H,3H,3H-pentafluoropentyl)oxy]-1,5-dioxobutane-2-sulfonate (Co(di-CF₂)₂),
177 Nickel 1,5-bis[(1H,1H,5H-octafluoropentyl)oxy]-1,5-dioxobutane-2-sulfonate (Ni(di-HCF₄)₂), Cobalt
178 1,5-bis[(1H,1H,5H-octafluoropentyl)oxy]-1,5-dioxobutane-2-sulfonate (Co(di-HCF₄)₂), Nickel 1,5-
179 bis[(1H,1H,7H-dodecafluoroheptyl)oxy]-1,5-dioxobutane-2-sulfonate (Ni(di-HCF₆)₂), Cobalt 1,5-
180 bis[(1H,1H,7H-dodecafluoroheptyl)oxy]-1,5-dioxobutane-2-sulfonate (Co(di-HCF₆)₂), and Sodium 1,5-
181 bis[(1H,1H,7H-dodecafluoroheptyl)oxy]-1,5-dioxobutane-2-sulfonate (Na(di-HCF₆)). All the surfactants
182 were synthesized and purified as described in ref [34-39]. Chemical structures of these surfactants are {R-
183 OCO-CH(-SO₃⁻)-CH₂-COO-R}_xM^{x+}, where M^{x+}=Co²⁺, Ni²⁺, or Na⁺, R=CF₃CF₂CH₂CH₂CH₂- for di-CF₂,
184 H(CF₂)₄CH₂- for di-HCF₄, or H(CF₂)₆CH₂- for di-HCF₆, **Figure S1** in Supplementary data).

185 Ultrapure water with a resistivity of 18.2 MΩ cm was obtained from a Millipore Milli-Q Plus
186 system. CO₂ was of > 99.995% purity (Taiyo Nippon Sanso Corp.). The structures of the steric models
187 and the length of surfactant molecules (in isolation) were calculated by MM2 (Molecular Mechanics
188 program 2) calculations (Chem 3D; CambridgeSoft Corp., Cambridge, MA).

189

190 2.2. Phase behaviour measurements

191 A high-pressure vessel with an optical window and moveable piston was used to observe phase
192 behavior of the surfactant/water/scCO₂ mixtures with varying pressures and temperatures. A detailed
193 description of the experimental apparatus and procedures for the measurements can be found elsewhere
194 [16-20,28,29].

195 The measurements of the water/surfactant/scCO₂ systems were performed at temperatures of 35 –
196 75 °C and pressures < 400 bar. The densities of CO₂ were calculated using the Span-Wagner Equation of

197 state (EOS) [41]. Pre-determined amounts of the surfactant and CO₂ (20.0g), where the molar ratio of
198 surfactant to CO₂ was fixed at 1.92×10^{-3} (i.e. 40 mM at 350 bar and 45 °C), 0.96×10^{-3} or 3.84×10^{-3}
199 were loaded into the variable-volume high-pressure optical cell, and the appropriate aliquot of water was
200 added through a six-port valve. The surfactant molar concentration varied between 20-40 mM in case of
201 the molar ratio of surfactant to CO₂ = 1.92×10^{-3} , as the inner volume of the cell was varied by changing
202 experimental pressure and temperature. The physical properties of the continuous phase of scCO₂ were
203 assumed to be equivalent to those of pure CO₂.

204

205 **2.3 High-Pressure viscosity measurements**

206 The relative viscosity of the surfactant/water/CO₂ solutions to pure CO₂ was measured with a
207 capillary-type high-pressure viscometer as shown in **Figure S2**. CO₂ high pressure cell, and pressure
208 gauges are the same as in the apparatus for phase behavior measurements. The cell, valves, joints, and all
209 SUS 316 tubes are temperature-controlled with a heater within ± 0.5 °C.

210 According to the Hagen-Poiseuille Equation (1) [42], viscosity is proportional to a differential
211 pressure between inlet and outlet of a capillary tube when a fluid flows through it.

212 Hagen-Poiseuille Equation
$$\eta = \frac{\pi P r^4 t}{8 \nu l} \quad (1)$$

213 where η is viscosity, P is differential pressure, r is inner radius of capillary, l is length of capillary, t is
214 time, and ν is volume of fluid. After a transparent single phase of the mixture was obtained, using the
215 same procedure as the phase behavior measurements, the valve between two 6-port valves (IDEX Health
216 & Science, Rheodyne 7010) was closed and the fluid was flowed into the capillary (inner diameter: 0.5
217 mm, length: 50 cm) by pumping at a flow rate of 0.658 ml/min with the high-pressure pump (Nihon
218 seimitsu kagaku co., ltd., NRX-01-H). The differential pressure between inlet and outlet of the capillary
219 was then measured with a high line pressure variable reluctance pressure Sensor (Validyne engineering,

220 DP363). Relative viscosity η_{rel} of a F-surfactant/water/CO₂ solution was calculated by dividing the
221 differential pressure of the surfactant solution by that of pure CO₂ as shown in the following equation.

$$222 \quad \eta_{\text{rel}} = \frac{\eta_{\text{CO}_2\text{-surf}}}{\eta_{\text{CO}_2}} = \frac{P_{\text{CO}_2\text{-surf}}}{P_{\text{CO}_2}} \quad (2)$$

223 Where η_{CO_2} is viscosity of pure CO₂, $\eta_{\text{CO}_2\text{-surf}}$ is viscosity of a water/surfactant/CO₂ system, P_{CO_2} is
224 differential pressure for pure CO₂, $P_{\text{CO}_2\text{-surf}}$ is differential pressure for a water/surfactant/CO₂ solution. All
225 the viscosity measurement was expected to be under laminar flow conditions. For example, the Reynolds
226 number (Re) was calculated as ~ 310 in the case of pure CO₂ at 75 °C and 350 bar from the equation $Re =$
227 $Q D_{\text{H}}/(\nu A)$, where Q is the volumetric flow rate, D_{H} is the hydraulic diameter of the capillary, ν is the
228 kinematic viscosity ($\nu = 8.9 \times 10^{-8} \text{ m}^2 \text{ s}^{-1}$)[43], A is the capillary's cross-sectional area [44]. Shear rate γ
229 was calculated as 890 s^{-1} from the equation $\gamma = 4Q D_{\text{H}}/(\pi r^3)$ [45].

230

231 **2.4 High-Pressure Small-Angle Neutron Scattering (HP-SANS) measurements and data analysis**

232 Due to the range of neutron wavelengths available, time-of-flight SANS is suitable for studying
233 the shapes and sizes of colloidal systems. High-pressure SANS (HP-SANS) is a particularly important
234 technique for determining aggregate nanostructure in supercritical CO₂. The HP-SANS measurements of
235 the D₂O/scCO₂ systems with di-HCF6 series with Ni, Co, and Na counterions were performed at 45 or 75
236 °C at various pressures. The LOQ time-of-flight instrument, and the SANS2D instrument, at the
237 Rutherford Appleton Laboratory at ISIS UK, were used in conjunction with a stirred high-pressure cell
238 (Thar). The path length of the cell and neutron beam diameter were both 10 mm. The measurements gave
239 absolute scattering cross sections $I(Q)$ (cm^{-1}) as a function of momentum transfer Q (\AA^{-1}), which is defined
240 as $Q = (4\pi/\lambda)\sin\theta$, where θ is the scattering angle. The accessible Q ranges were 0.007-0.22 \AA^{-1} for LOQ
241 and 0.002-1 \AA^{-1} for SANS2D arising from an incident neutron wavelength, λ , of 2.2-10 \AA . The data were
242 normalized for transmission, empty cell, solvent background, and pressure induced changes in cell volume
243 as before [28,29].

244 Pre-determined amounts of D₂O and surfactant, where the molar ratios of surfactant to CO₂ were
245 fixed at 1.92×10^{-3} (= 40 mM at the appropriate experimental condition, respectively), were loaded into
246 the Thar cell. Then, CO₂ (11.3g), was introduced into the cell using a high-pressure pump, and the
247 surfactant/D₂O/CO₂ mixture was pressurized to 350 bar at 45 or 75 °C by decreasing the inner volume of
248 the cell. With vigorous stirring, visual observations were carried out to identify a transparent single-phase
249 (W/CO₂ μEs). Finally, the HP-SANS experiments were performed for the single-phase W/CO₂ μEs. Due
250 to the systems being dilute dispersions (volume fractions typically 0.12 or less), the physical properties
251 of the continuous phase of scCO₂ were assumed to be equivalent to those of pure CO₂.

252 Scattering length densities of surfactants, CO₂ and D₂O were calculated (section S3 in
253 supplementary information). The shells of the surfactant/D₂O/CO₂ μEs were estimated to be composed
254 of the fluorinated tails **R** in **Fig. S1**, and the scattering length density (SLD), ρ_{shell} , was calculated as 3.50
255 $\times 10^{10} \text{ cm}^{-2}$ for the fluorinated chain H(CF₂)₆- from Equation (S1) in supplementary data. On the other
256 hand, aqueous cores with D₂O were suggested to contain the hydrophilic parts of the surfactants, which
257 means the other molecular parts except the fluorinated chain. Then the SLD values of cores, ρ_{core} , were
258 estimated as $4.76\text{-}5.85 \times 10^{10} \text{ cm}^{-2}$ for Ni and $4.77\text{-}5.86 \times 10^{10} \text{ cm}^{-2}$ for Co at $W_0 = 5\text{-}20$, and increased
259 with D₂O content, namely W_0 . For the SLD calculation of the shell and the cores mass densities of 1H-
260 perfluorohexane, dimethylsuccinate, Nickel sulfonate, and Cobalt sulfonate at 25 °C were employed as
261 1.68 g cm^{-3} , 1.09 g cm^{-3} , 1.80 g cm^{-3} , and 1.77 g cm^{-3} , respectively [46]. As ρ_{shell} was far from ρ_{CO_2} (2.29
262 $\times 10^{10} \text{ cm}^{-2}$ at 45 °C and $2.02 \times 10^{10} \text{ cm}^{-2}$ at 75 °C), SANS from the D₂O/F-surfactant/CO₂ μEs was
263 assumed to be from both core and shell, the so-called aqueous core/fluorocarbon shell contrast.

264 For model fitting data analysis, the W/CO₂ μE droplets were treated as spherical, cylindrical or ellipsoidal
265 particles with Schultz distributions in core radius and length [47]. The polydispersities in those radii and
266 lengths were fixed at 0.2 as found in typical W/O μEs [48]. Full accounts of the scattering laws are given
267 elsewhere [36-39,47,49]. To account for weak attractive interactions between microemulsion droplets,
268 square well structure factor ($S(Q)$) was also employed. The perturbation parameter is $\varepsilon = \Delta/(\sigma+\Delta)$, where

269 Δ and σ are the width of the attractive square well pair potential and the hard core diameter ($\sigma = 2R_c$),
270 respectively. The attractive stickiness, τ , is defined as

$$271 \quad \tau = \frac{1}{12\varepsilon} \exp(U_0/kT) \quad (3)$$

272 τ is a function of both the perturbation parameter and the interaction strength in terms of the depth of
273 the well, U_0 . From the definition, that smaller τ means stronger attraction.

274 Data were fit to the models described above using the SasView small-angle scattering analysis
275 software package (<http://www.sasview.org/>). The fitted parameters were the core radius R_{f-cyl} and the
276 length L_{f-cyl} for core/shell cylindrical particles; these values were initially estimated by preliminary
277 Guinier analyses (L_{g-cyl} , R_{g-cyl}) [29,50]. During the fitting analysis shell thickness was kept constant at 7.4
278 Å as estimated from the tail structure of H(CF₂)₆- by the MM2 simulation.

279

280 **2.5. Surface pressure measurements**

281 Surface pressure-area isotherms were measured on a KSV minitrough (KSV 2000, KSV
282 Instruments Ltd.) equipped with a platinum Wilhelmy plate, at 35 °C. In each experiment, a chloroform
283 solution containing surfactant was spread on the water surface. 15 minutes were allowed for solvent
284 evaporation before compression. The barrier was moved at a speed of 10 mm min⁻¹.

285

286

287 3. Results and Discussion

288 3.1 Effects of counterion, water content, pressure, and fluorinated tail on microemulsion formation

289 Above a threshold phase boundary pressure (P_{trans}) the surfactant/water/ CO_2 mixtures formed
290 transparent single-phases (i.e. Winsor-IV W/ CO_2 μE). On the other hand, transparent phase change into
291 a turbid macroemulsion or a precipitated hydrated phase below P_{trans} (i.e. lower CO_2 density). The P_{trans}
292 and the CO_2 density for surfactant/W/ CO_2 mixtures were determined for various W_0 values and
293 temperatures (35-75 °C), as shown in Supplementary data (**Figures S3-S9**). **Figure 1** displays P_{trans} for
294 surfactant/water/ CO_2 mixtures with $W_0 = 10$ or 20 at $[\text{surfactant}]/[\text{CO}_2] = 1.92 \times 10^{-3}$. In this Figure, 1ϕ and
295 2ϕ represent transparent single-phase and two-phase systems, respectively. Some of these surfactants at
296 $[\text{surfactant}]/[\text{CO}_2] = 1.92 \times 10^{-3}$ were not completely dissolved in CO_2 at any pressure and temperature
297 studied. For example, the mixtures for $\text{Co}(\text{di-CF}_2)_2$ at $W_0 > 5$, $\text{Co}(\text{di-HCF}_4)_2$ at $W_0 > 15$, and $\text{Ni}(\text{di-}$
298 $\text{HCF}_4)_2$ at $W_0 > 10$ were always two-phase under the experimental conditions studied.

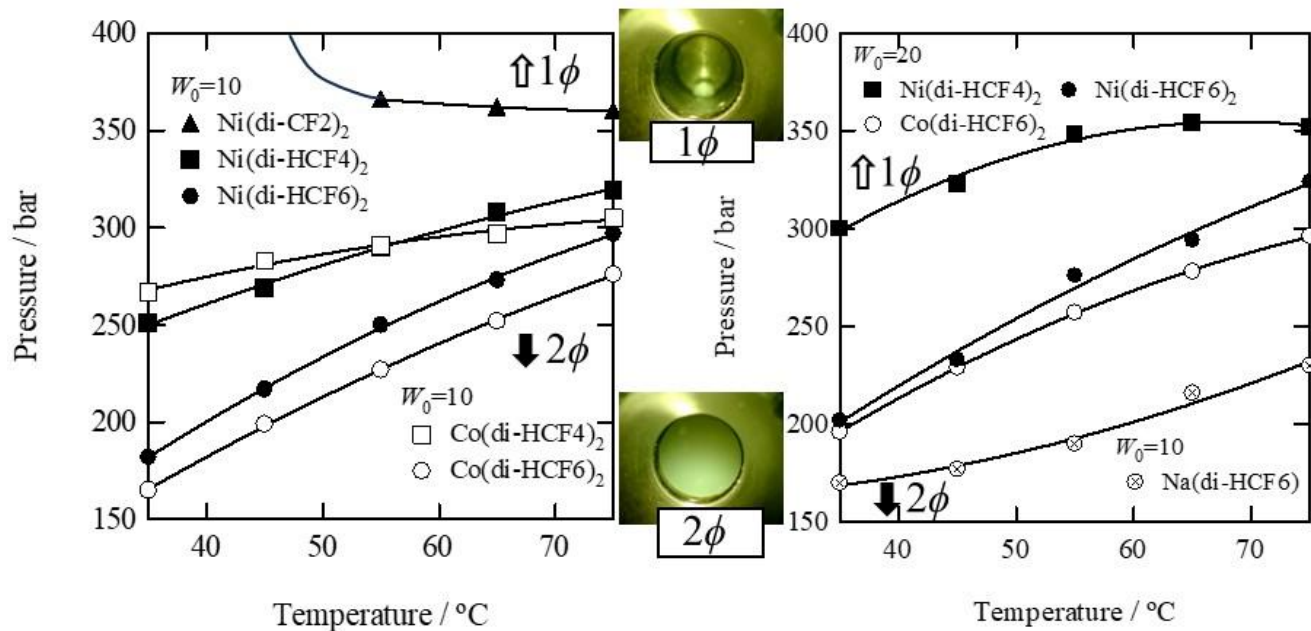
299 Comparing surfactants with the same counterion, it is clear that longer fluorinated tails lead to
300 lower P_{trans} . This may be attributed to increased CO_2 -philicity of surfactants bearing longer fluorinated
301 tails, allowing for increased CO_2 solvation and stabilization of microemulsions at lower pressures P_{trans}
302 [16-22]. Looking at surfactants with the same CO_2 -philic tails, surfactants can likely form a single phase
303 at lower pressures with smaller atomic number counterions ($\text{Na} < \text{Co} < \text{Ni}$) or stronger ionization tendency
304 ($\text{Na} > \text{Co} > \text{Ni}$). This trend may be linked to lower W/ CO_2 interfacial tensions, higher counterion
305 dissociation and/or higher hydrogen bonding efficiency with the water of the headgroups [3,26,27,38,39].

306 In most cases, P_{trans} tends to increase with temperature. However, as indicated by **Figures S3-S9**
307 the phase boundary instability is better thought of in terms of CO_2 density rather than P_{trans} . This has been
308 reported in earlier studies [16-22], and was attributed to solubility in scCO_2 which is a linear function of
309 CO_2 density, rather than pressure [16-22].

310 On the other hand, as shown in **Figure S3-S9** P_{trans} increases with W_0 for all the surfactants studied.
311 Increasing the water loading induces droplet growth, which may lead to stronger inter-droplet interaction.
312 Hence higher pressures (or CO_2 density) are required to solvate reverse microemulsion droplets with more

313 CO₂ molecules (i.e. a higher CO₂ density or pressure), to prevent aggregation and fusion. As shown in
314 **Figures S10** and **S11** the effect of surfactant concentration on P_{trans} at $W_0 = 10$ was also examined:
315 doubling concentration increases P_{trans} by 6-73 bar. Increasing the surfactant and water concentration
316 together (i.e. at fixed W_0) may be expected to increase attractive interactions, which would destabilize the
317 microemulsions.

318



320

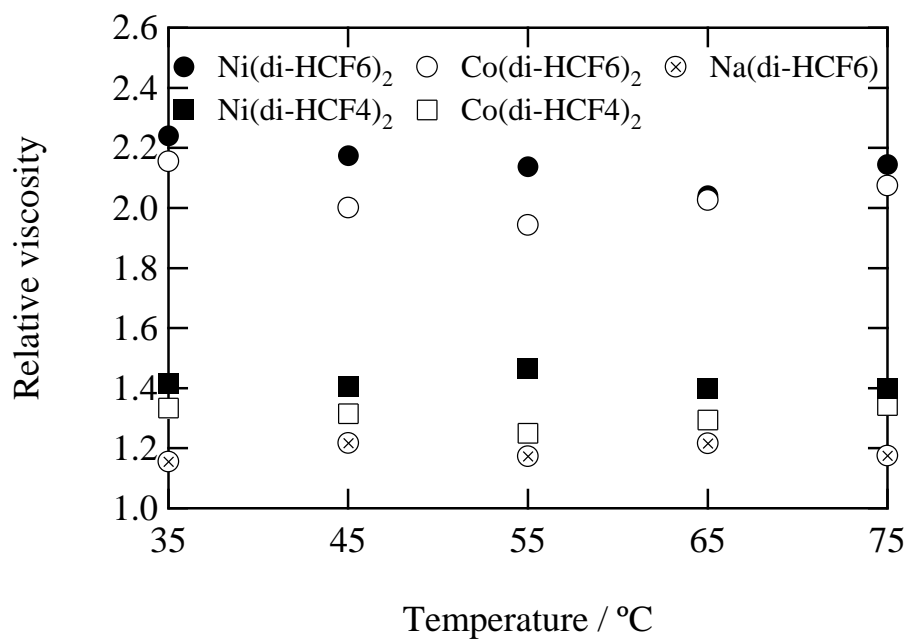
321 **Figure 1.** Phase boundary pressures between transparent “micro”emulsion (1ϕ) and turbid
 322 “macro”emulsion (2ϕ) systems as a function of temperature for surfactant/W/ CO_2 mixtures with $W_0 = 10$
 323 and 20 and $[\text{surfactant}]/[\text{CO}_2]$ of 1.92×10^{-3} (Co^{2+} and Ni^{2+}) and 3.84×10^{-3} (Na^+). Photographs show
 324 appearance of 1ϕ and 2ϕ systems, under stirring, in the high-pressure cell.

325

326 **3.2 Viscosity enhancement of CO₂ by low fluorine-content surfactants**

327 To examine the ability of these surfactant/W/CO₂ systems to increase the viscosity and thicken CO₂, the
328 relative viscosities η_{rel} were measured at 350 bar (**Figures S12-S14**). **Figure 2** shows η_{rel} for systems at
329 $W_0=10$. To compare the data at the same surfactant anion concentration, [surfactant]/[CO₂] was 3.84×10^{-3}
330 for Na⁺, but 1.92×10^{-3} for Co²⁺ and Ni²⁺. [The measurement of η_{rel} with M(di-CF₂)₂ $W_0=10$ was not
331 possible in this rig, since $P_{\text{trans}} > 350$ bar.]

332



334

335 **Figure 2** Relative viscosity η_{rel} as a function of temperature for $M(\text{di-HCF}n)_x$ ($n = 4$ or 6 , $M = \text{Na}^+$, Co^{2+}
 336 or Ni^{2+})/W/ CO_2 mixtures with $W_0=10$ at 350 bar. The ratios $[\text{surfactant}]/[\text{CO}_2]$ were 3.84×10^{-3} for Na^+ ,
 337 and 1.92×10^{-3} for Co^{2+} and Ni^{2+} . Shear rates were in the $10\text{-}1000 \text{ s}^{-1}$ range.

338

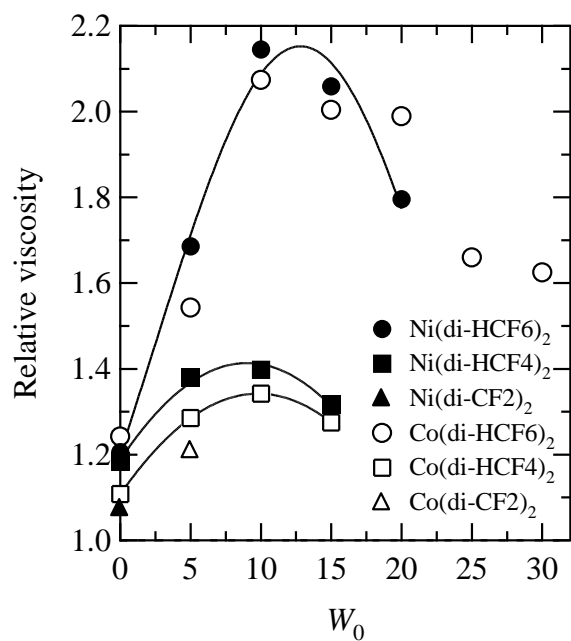
339

340 Over the range 35-75 °C temperature has only a marginal effect on η_{rel} . Longer tail fluorinated surfactants
341 Ni(di-HCF6)₂ and Co(di-HCF6)₂ gave η_{rel} 1.94-2.24, notably higher than 1.5 for the shorter F-tail
342 analogues Ni(di-HCF4)₂ and Co(di-HCF4)₂. Surfactants with Ni²⁺ counterions gave higher η_{rel} compared
343 those with Co²⁺. It is interesting to note that the Na⁺ for the longer fluorinated tails became very low
344 by exchanging the divalent counterion Ni or Co for the monovalent Na-HCF6 gave the lowest η_{rel} values.
345 These results indicate that long fluorinated tails $\geq C_6$ and divalent counterions are important feature of
346 these surfactants for CO₂-thickening. A plausible explanation for this chemically specific behavior is that
347 anisotropic, rod-shaped micelles might be formed in the Ni(di-HCF6)₂ and Co(di-HCF6)₂ systems.
348 Section 3.3 below details structural studies of the micelles/microemulsions in these systems using SANS.

349 **Figure 3** shows the variation of η_{rel} for surfactant/water/CO₂ mixtures as a function of W_0 at 75 °C
350 and 350 bar. On increasing W_0 up to 10, η_{rel} was found to increase especially for the longer tail surfactants.
351 On the other hand, the η_{rel} gradually decreased for systems at $W_0 > 10$. One possible explanation for these
352 trends is that reverse micelle self-assembly structure changes from spherical to rod-like as a function of
353 W_0 , with maximum anisotropy, and hence viscosity occurring about $W_0 \sim 10$. In earlier studies with hybrid
354 H-F surfactants, long rod-like reverse micelles with lengths of $> 250 \text{ \AA}$ were only formed in scCO₂ at W_0
355 ~ 10 [29]. Under those conditions the H-F hybrid surfactants reached an effective packing parameter (EPP)
356 of 1.4-1.7, consistent with stabilization for rod-like micelles. Further, the presence of cylinder (rod)
357 micelles was confirmed by SANS [27,38,39].

358 The effect of surfactant concentration ([surf]) at constant $W_0 = 10$ on η_{rel} in **Figure S14**. For all
359 surfactants and experimental conditions tested, η_{rel} clearly increased with [surf], with the effects being
360 greater for the longer F-chain surfactants M(di-HCF6)₂. This would be consistent with longer rod-like
361 micelles with the M(di-HCF6)₂ series compared to M(di-HCF4)₂ analogues.

362



363

364 **Figure 3** Relative viscosities as a function of W_0 for surfactant/ W / CO_2 mixtures at 75 °C and 350 bar. The

365 ratio of [surfactant]/[CO_2] was fixed at 1.92×10^{-3} . Shear rates were in the 10-1000 s^{-1} range.

366

367 3.3 Structural studies by High Pressure SANS

368 SANS $I(Q)$ profiles were measured for water/CO₂ μ Es at [surfactant]/[CO₂] of 1.92×10^{-3} , 350
369 bar, 45 and 75 °C, and different W_0 values. For Ni(di-HCF6)₂ and Co(di-HCF6)₂ SANS profiles at 75 °C
370 and 350 bar are shown in **Figure 4**. The SANS data for Na(di-HCF6) at 75 °C and 350 bar and Co(di-
371 HCF6)₂ at 45 °C and 350 bar can be found in **Figures S19-S20** (Supplementary data).

372 In the low Q region (typically in the case of droplet μ Es $< 0.01 \text{ \AA}^{-1}$), the SANS may scale as $I(Q)$
373 $\sim Q^{-D}$, where D is a characteristic “fractal dimension”; hence, the gradient of a log-log plot will be $-D$. In
374 the case of non-interacting spheres, D should be zero in this low Q region, whereas $D = 1$ for cylinders
375 and 2 for disks [29,49,50]. When viewed in this way, the SANS profiles for Co(di-HCF6)₂ and Ni(di-
376 HCF6)₂ show $D = 1$, and 2 for Na(di-HCF6), suggesting the presence of rod-like and disk-like particles,
377 respectively. Using appropriate Guinier plots, the radius of gyration R_g , cylinder radius (or disk radius)
378 R_{g-cyl} and length (or disk thickness) L_{g-cyl} , sphere radius R_{g-sph} of water/CO₂ μ Es can be estimated (**Figures**
379 **S15-S18**) and are listed in **Table S1**.

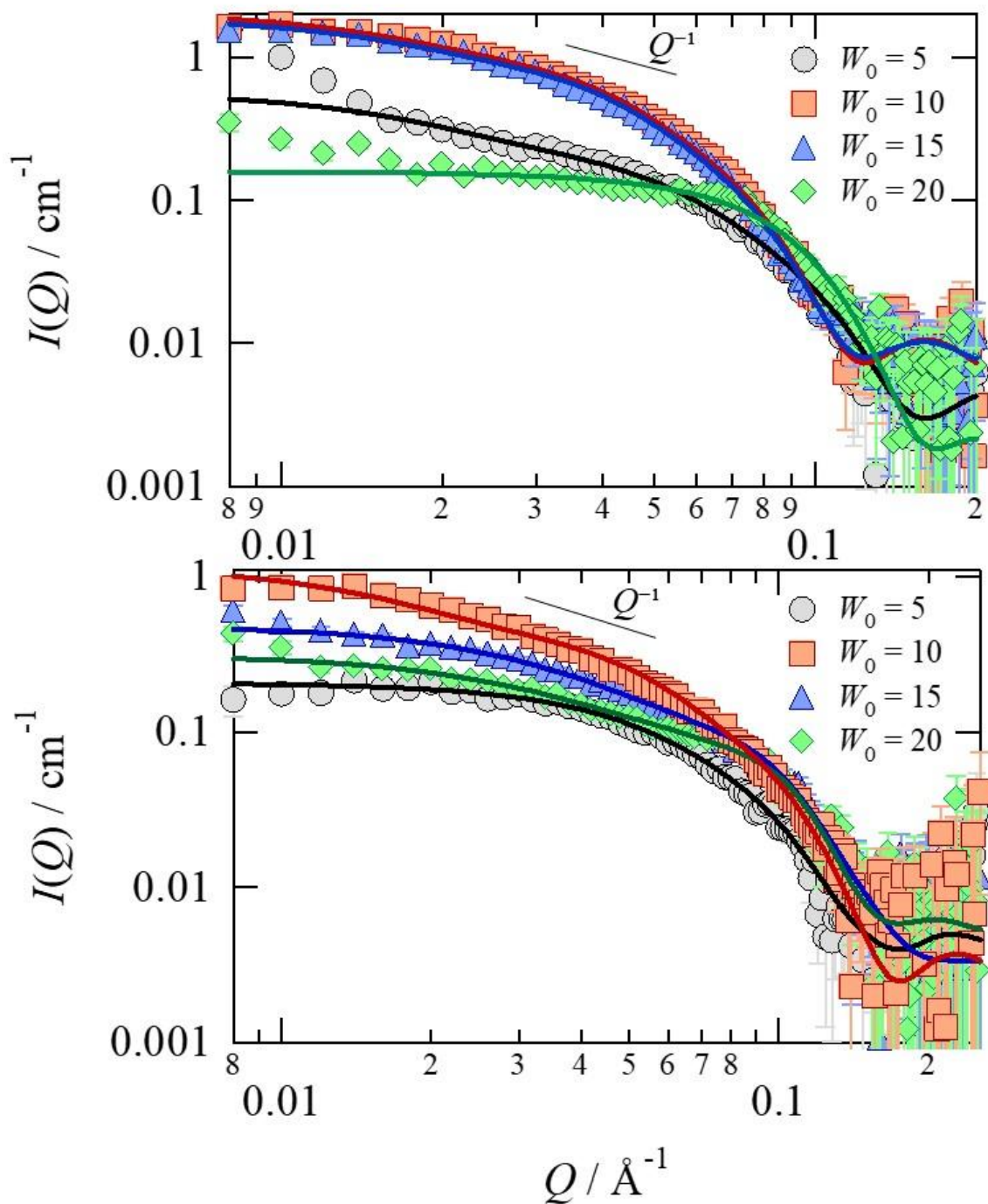
380 These SANS data were analyzed in detail by model fitting to various form factor models ($P(Q)$)
381 to gain information on the size and morphology of the reverse micelles/microemulsion. As initially
382 indicated based on the logarithmic scaling (Q^{-1} or Q^{-2}), most SANS profiles for these W/CO₂
383 microemulsions were best-fitted by a form factor for anisotropic particles (which reports on cylinders for
384 aspect ratio ($L_{f-cyl}/(2R_{f-cyl}) \gg 1$, and disks with ($L_{f-cyl}/(2R_{f-cyl}) < 1$). It was found that a small contribution
385 from $S(Q)$, based on a square-well potential, accounting for additional weak attractions, helped improve
386 the fit quality in the low Q regions. The initial values of R_{g-cyl} and L_{g-cyl} obtained by trail Guinier plot
387 analyses (**Figures S15-S18, Table S1**) were used as the starting points for the curve fitting. In **Figure 4**
388 the solid lines are the best fitted functions for the cylinder $P(Q)$ with a polydispersity index of 0.2 and the
389 $S(Q)$ data. The values of R_{f-cyl} and L_{f-cyl} are given in **Table 1** and **Table S2** (Supplementary data). In the
390 case of the W/CO₂ mixture with Co(di-HCF6)₂ at $W_0=20$ and 75 °C, the aspect ratio $L_{f-cyl}/(2R_{f-cyl})$ was ~ 1 ,
391 suggesting spherical particles. The SANS data was also well-fitted with the theoretical curve of spherical
392 particles with radius of 19.6 \AA as shown in supplementary data (Fig. **S21**).

394 **Table 1** Fit parameters obtained from model fitting of SANS profiles for M(di-HCF6)_x/water/CO₂ reverse
395 micelles/microemulsions. Radius (R_{f-cyl}) and length (L_{f-cyl}) for cylinder particle $P(Q)$; volume fraction (ϕ);
396 aspect ratio ($L_{f-cyl}/(2R_{f-cyl})$); micelle concentration (C_{agg}); aggregation number (N_{agg}); effective water/CO₂
397 interfacial area ($A_{w/C}$). Also given is the effective packing parameter (EPP) for surfactant molecules. The
398 values of C_{agg} , N_{agg} , $A_{w/C}$, and EPP were estimated from Equations (5)-(10) using R_{f-cyl} , L_{f-cyl} , and ϕ . The
399 value of [surfactant]/[CO₂] was 1.92×10^{-3} for all surfactant systems except Na(di-HCF6), except for
400 Na(di-HCF6) which was 3.84×10^{-3} .

M^{x+}	$T / ^\circ C$	W_0	$R_{f-cyl} / \text{\AA}$	$L_{f-cyl} / \text{\AA}$	$L_{f-cyl} / (2R_{f-cyl})$	ϕ	$C_{agg} / (\text{mM})$	N_{agg}	$A_{w/C} / \text{\AA}^2$	EPP
Co ²⁺	75	5	13.8 ± 0.3	238 ± 20	5.95	0.048	0.22 ± 0.03	180 ± 23	121 ± 28	1.32 ± 0.15
		10	23.3 ± 0.1	266 ± 9	4.58	0.051	0.08 ± 0.00	483 ± 22	88 ± 7	1.20 ± 0.05
		15	24.8 ± 0.2	264 ± 9	4.33	0.055	0.09 ± 0.00	465 ± 21	97 ± 8	1.19 ± 0.05
		20	17.8 ± 1.0	37 ± 5	1.03	0.059	1.36 ± 0.34	29 ± 7	208 ± 87	1.47 ± 0.25
	45	5	18.9 ± 0.1	123 ± 2	2.62	0.048	0.23 ± 0.01	174 ± 5	97 ± 5	1.29 ± 0.03
		10	22.9 ± 0.1	194 ± 3	3.45	0.051	0.12 ± 0.00	339 ± 7	92 ± 4	1.22 ± 0.02
Ni ²⁺	75	5	13.6 ± 0.3	92 ± 4	2.54	0.048	0.60 ± 0.05	67 ± 5	134 ± 19	1.42 ± 0.09
		10	14.4 ± 0.1	267 ± 20	6.47	0.051	0.22 ± 0.02	185 ± 16	138 ± 22	1.30 ± 0.11
		15	12.6 ± 0.2	76 ± 3	2.27	0.055	1.15 ± 0.08	35 ± 2	202 ± 24	1.46 ± 0.08
		20	18.9 ± 1.4	24 ± 4	0.74 (Disc)	0.059	1.81 ± 0.58	22 ± 7	233 ± 123	1.52 ± 0.32
Na ⁺	75	5	10.9 ± 0.1	10.1 ± 0.1	0.68 (Disc)	0.052	10.4 ± 0.29	8 ± 0	186 ± 8	2.11 ± 0.04
		10	15.5 ± 0.3	22.0 ± 0.6	0.80 (Disc)	0.059	3.09 ± 0.22	26 ± 2	141 ± 17	1.63 ± 0.08
		15	21.9 ± 0.2	18.9 ± 0.1	0.58 (Disc)	0.067	1.10 ± 0.03	73 ± 2	78 ± 3	1.50 ± 0.02

401

402



403

404 **Figure 4.** SANS profiles for M(di-HCF6)₂/D₂O/CO₂ mixtures with different W_0 values at 75 °C and 350
 405 bar. The ratio [surfactant]/[CO₂] was fixed at 1.92×10^{-3} . The counterion M is (top) Co²⁺ or (bottom) Ni²⁺.
 406 Fitted curves were based on a model incorporating a Schultz distribution of polydisperse cylinder particles
 407 with core (D₂O and the hydrophilic group) and a shell (fluorinated tails). A contribution from the square-
 408 well structure factor $S(Q)$ was also included in the model.

410 Visual phase behavior observations as a function of P , T and W_0 , showed transparent single-phases
 411 above the phase boundary pressures P_{trans} , consistent with W/CO₂ microemulsion phases. However, there
 412 is a possibility that small amounts of water separated from the reverse micelle/CO₂ systems, which are
 413 difficult to observe by the naked eye. For both surfactants in **Figure 4**, the measured $I(Q)$ profiles at
 414 $W_0=15-20$ were lower than those at $W_0=10$. This would be consistent with formation of Winsor-II phases
 415 (namely a W/CO₂ microemulsion having a separated excess water) at these higher W_0 values (or partially
 416 formed a W/CO₂ reverse-type liquid crystal [19,20]). To clarify whether reverse micelles grew regularly
 417 with increasing W_0 , the ratio of volume-to-surface area ($v_{\text{core}}/s_{\text{core}}$) of aqueous core was calculated using
 418 $R_{\text{f-cyl}}$ and $L_{\text{f-cyl}}$, and plotted as a function of W_0 (**Figure S22**). In previous study [28,29], with a strong
 419 surfactant such as the FC-HC hybrid FC6-HC4, this value $v_{\text{core}}/s_{\text{core}}$ tends to increase with W_0 , consistent
 420 with the formation of Winsor-IV microemulsions (i.e., all the added water is dispersed, with no excess
 421 water phase as for a Winsor-II system). In the case of Winsor-IV systems Equation (4) applies,

$$422 \quad \alpha(p) (v_{\text{core}}/s_{\text{core}}) = (v_{\text{head}} N_{\text{agg}} + v_{\text{w}} W_0 N_{\text{agg}}) / (A N_{\text{agg}}) = (v_{\text{head}}/A) + (v_{\text{w}}/A) W_0 \quad (4)$$

424 where $\alpha(p) = 1 + 2p^2$, p is polydispersity index, v_{w} is the volume of water molecule, N_{agg} is the aggregation
 425 number, v_{head} is the volume of surfactant headgroup and A is the area per surfactant molecule. The values
 426 of s_{core} and v_{core} were calculated using $s_{\text{core}} = 2\pi R_{\text{f-cyl}} L_{\text{f-cyl}} + 2\pi R_{\text{f-cyl}}^2$ and $v_{\text{core}} = \pi R_{\text{f-cyl}}^2 L_{\text{f-cyl}}$ for cylindrical
 427 particles. Referring to **Figure S22**, the surfactants Co(di-HCF6)₂ and Ni(di-HCF6)₂ did not show any
 428 significant increase in $v_{\text{core}}/s_{\text{core}}$ above $W_0 = 10$. This would be consistent the additional water added above
 429 $W_0 = 10$ not being taken up into reverse micelles, and Winsor-II systems (or W/CO₂ reverse-type liquid
 430 crystals [17-20]). The presence of shoulders in the SANS profiles at $W_0=20$, which are indicated by arrows
 431 in **Figure S23**, may be interpreted as Bragg-type peaks, owing to liquid crystalline ordering. SANS
 432 profiles for D₂O/CO₂ microemulsions with Co(di-HCF6)₂ and Ni(di-HCF6)₂ at $W_0 = 20$, 75 °C and 350
 433 bar were found to show such Bragg peaks (as pointed by arrows in **Figure S23**). Di-chain surfactants with
 434 single head group, structurally akin to lipids [51,52] are known to form liquid crystals: for example, and
 435

436 not limited to, fluorinated double-tail surfactants such as di-HCF6 are found to form lamellar liquid
437 crystals in W/CO₂ mixtures with high W_0 values of > 10 [17-20]. Based on these possible Bragg peaks
438 the layer spacings were estimated as 85 Å for Co(di-HCF6)₂ and 68 Å for Ni(di-HCF6)₂. Based on the
439 assumption that the hydrophobic tails are 7.4 Å (length of H(CF₂)₆- chain), this suggests layers of water
440 + hydrophilic groups to be ~70 Å for Co(di-HCF6)₂ and ~53 Å for Ni(di-HCF6)₂. These thicknesses
441 would be consistent with electrostatic repulsion between charged head groups and neighboring
442 counterions on opposing surfaces.

443 For W_0 values of 5-10 the surfactants with divalent counterions with Co(di-HCF6)₂ and Ni(di-HCF6) gave
444 rise to the greatest anisotropy and micellar elongation, in terms of the aspect ratio ($L_{f-cyl}/(2R_{f-cyl})$). In more
445 detail, the micellar morphology of these two surfactants evolved from short rods at $W_0=5$, to much longer
446 rods at $W_0=10$, decaying to short rods at $W_0=15$, and then spheres or oblates at $W_0=20$. These changes in
447 micellar structure, with long rods at $W_0=10$, map on to the η_{rel} behavior seen in **Figures 2** and **3**. Finally,
448 formation of the longest rod-like reverse micelles $L_{f-cyl} \sim 260$ Å lead to $\eta_{rel} \sim 2$. This represents the first
449 observation of rod-like reverse micelles in CO₂ at a temperature of 75 °C, which is close to real reservoir
450 conditions. To explore further how to control reverse micelle morphology, to generate the longest rods
451 (worm-like or thread-like ones), the next section considers the effects of counterion, W_0 , and surfactant
452 concentration on aggregation number (N_{agg}) and effective packing parameter (EPP).

453

454 3.4 Micellar structure and surfactant architecture

455 To investigate the aggregation properties of these surfactants in scCO₂, the aggregation number
456 (N_{agg}) and area occupied per molecule at the W/CO₂ μ E surface ($A_{C/W}$) were calculated via the following
457 Equations [29,53].

$$458 \quad N_{agg} = C_{surf}/C_{agg} \quad (5)$$

$$459 \quad A_{C/W} = s_{core}/N_{agg} \quad (6)$$

$$460 \quad C_{agg} = (V_{D2O} C_{D2O} + V_{head} C_{surf})/(V_{core}) = C_{surf} (V_{D2O} W_0 + v_{head} N_A)/(v_{core} N_A) \quad (7)$$

461 where C_{surf} , C_{agg} and C_{D2O} are molar concentrations of surfactant, micelle, and D₂O, respectively. N_A is
462 the Avogadro number, V_{D2O} , V_{head} , and V_{core} are molar volumes of D₂O, surfactant headgroup and aqueous
463 core, v_{core} and v_{head} are volumes per aqueous core ($V_{core} = v_{core} N_A$) and headgroup ($V_{head} = v_{head} N_A$),
464 respectively. The values of v_{head} are shown in the section **S2** in Supplementary data. The assumption
465 implicit in these calculations is that all surfactant molecules are adsorbed at the W/CO₂ interface. In real
466 W/CO₂ microemulsions, it is likely that a small fraction of the surfactant molecules will partition away
467 from the interface owing to low background solubilities in water and CO₂. However, this is estimated to
468 be negligible compared with total number of associated surfactant molecules (9.6×10^{-2} mol%), taking
469 into account only very low critical microemulsion concentrations in scCO₂ for ionic F-surfactants,
470 typically $< 10^{-4}$ mol % [3,20,26-29,38,39,54,55]. The values of C_{agg} , N_{agg} , and $A_{C/W}$ are listed in **Table 1**,
471 and changes in N_{agg} as a function of W_0 are displayed in **Figure S25**. The figures also include data for
472 W/CO₂ microemulsions with the hybrid surfactant M-F7H4 (M=Li⁺, K⁺, Na⁺) [3,26,27], FC6-HC*n*
473 [28,29], double-tail surfactants *n*FG(EO)₂ (*n* = 4 and 8) [20], Ni(di-HCF4)₂ [38,39], and regular W/O
474 microemulsions with AOT in *n*-heptane [54]. The broken circle in the plot indicates conditions at which
475 long rod-like reverse micelles with length > 250 Å formed.

476 As expected, owing to growth and elongation of reverse micelles/microemulsion droplets with
477 increasing W_0 , the N_{agg} values increase with W_0 as shown in **Figure S25**. Such an increasing trend of N_{agg}
478 with W_0 was also reported in the different W/CO₂ and W/O microemulsions stabilized by other surfactants
479 [3,20,26-29,38,39,54,55]. The gradient becomes steeper for rod-like reverse micelles (see the broken

480 circle for the long rod-like reverse micelle region). On the other hand, for Co(di-HCF6)₂ and Ni(di-
 481 HCF6)₂, N_{agg} drastically decreases as the micelle morphology evolves from rod-like to globular in the
 482 single phase Winsor-IV systems at $W_0 = 10$, and then into two-phase Winsor-II or co-existing liquid crystal
 483 systems at $W_0 \geq 15$ (**Table 1**).

484 N_{agg} values decrease in the order of $Na^+ < Ni^{2+} < Co^{2+}$. Regarding $A_{W/C}$ the value for Co^{2+} was the
 485 lowest, perhaps owing to stronger interactions between Co^{2+} ions with the $-SO_3^-$ headgroups leading to
 486 greater electrostatic shielding of $-SO_3^-$ - $-SO_3^-$ repulsions. Similarly, at the air/water interface and 35 °C
 487 the effective area per surfactant anion for Co(di-HCF6)₂ was also lower compared with that for Ni(di-
 488 HCF6)₂ (**Figure S24** and **Table S3**). In addition, the $A_{C/W}$ values for Co^{2+} and Ni^{2+} ions were less than
 489 double those for Na^+ although the divalent-ion analogues have two surfactant ions per molecule. It
 490 suggests that the larger $A_{C/W}$ values for Na^+ ion does not arise principally owing to steric hindrance
 491 between the fluorinated tails solvated with CO_2 , but rather stronger $-SO_3^-$ - $-SO_3^-$ electrostatic headgroup
 492 interactions and weaker screening by Na^+ ions. Interestingly, the $A_{C/W}$ values for Na(di-HCF6) are quite
 493 close to those of other the double F-tail anionic surfactants with Na^+ counterions, ($nFG(EO)_2$ and
 494 $nFS(EO)_2$) as mentioned above [16,20,49].

495 Generation of rod-like reverse micelles could be accounted for by changes in critical packing
 496 parameter (CPP) (i.e. spontaneous packing parameter, SPP) and/or hydrophilic- CO_2 -philic balance (HCB).
 497 These packing indices can be thought of as a measure of the molar Gibbs free energy difference ($\Delta \bar{G}_{sphere \rightarrow cylinder}$) [56] between the endcaps (i.e. semi-spheres) and the cylindrical body of rod-like reverse
 498 micelles. Based on this concept, the Co^{2+} surfactant would generate a more negative $\Delta \bar{G}_{sphere \rightarrow cylinder}$ ($= \bar{G}_{cyl-body} - \bar{G}_{endcap}$), implying that the surfactant molecules prefer cylindrical, rather than endcap packing.

501 According to theory [57-59] SPP can be obtained by

$$502 \quad SPP = v_{tail}/(A_0 l_{tail}) \quad (8)$$

503 where v_{tail} and l_{tail} are hydrophobic tail volume and length, respectively (the same meanings as in the
 504 expression for [59]). Entropy is taken into account by the fact that the preferred area per molecule A_0
 505 minimizes the free energy of the surfactant film. According to this approach, reverse micelles would be
 506 obtained with $SPP > 1$ (reversed cores form if the surfactant tails orient upward) to ~ 1 (cylindrical). In
 507 the case of W/CO₂ microemulsions, the A_0 and v_{tail} values used to generate EPP should be calculated
 508 taking into account solvation of the head and tail groups with water and CO₂. If the hydrophobic part is
 509 assumed to be a truncated cone, the volume would be [29,53]

$$510 \quad v_{\text{tail}} = l_{\text{tail}} \{A_{C/W} + A_{\text{tail}} + (A_{C/W} A_{\text{tail}})^{0.5}\} / 3 \quad (9)$$

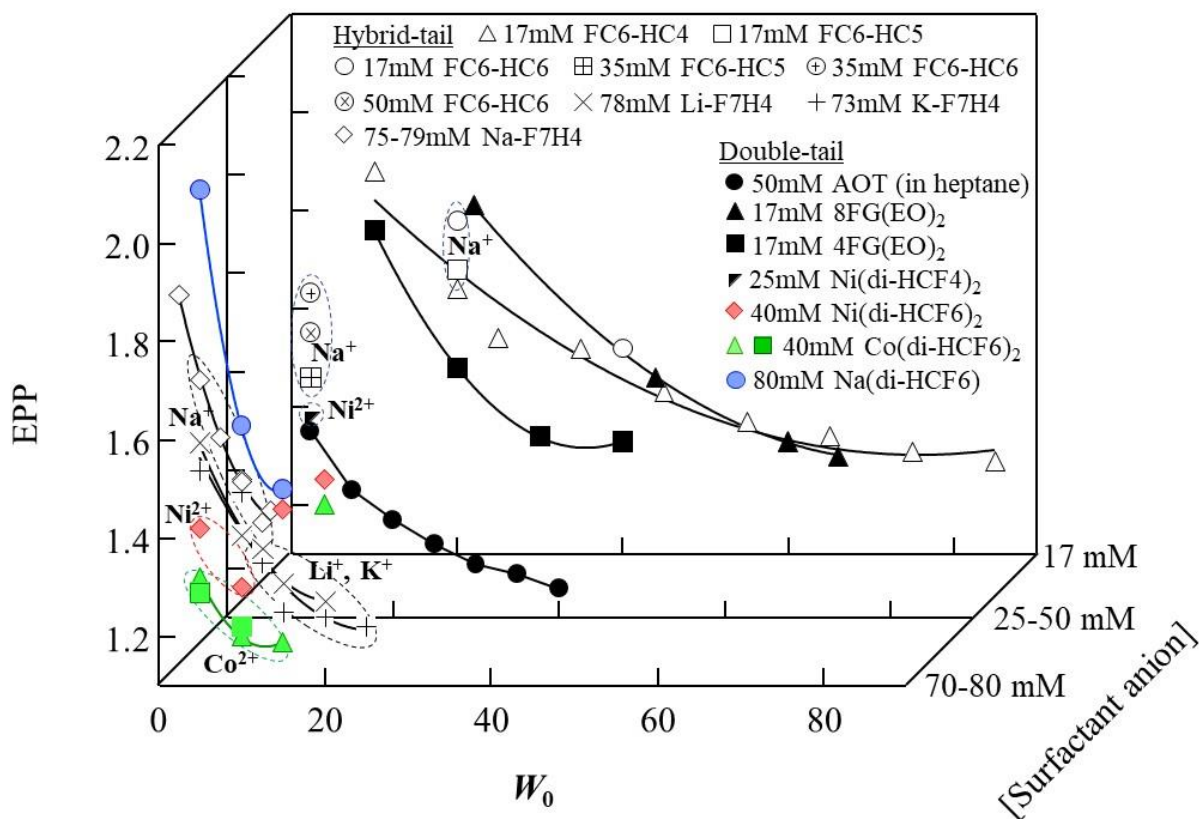
511 where A_{tail} is area per hydrophobic tail terminus, respectively. For the calculation of EPP in W/CO₂
 512 microemulsions, when A_0 is replaced by $A_{C/W}$, Eq. (8) can be simply expressed as

$$513 \quad EPP = \{s_{\text{agg}} + s_{\text{core}} + (s_{\text{agg}} s_{\text{core}})^{0.5}\} / (3s_{\text{core}}) \quad (10)$$

514 where s_{agg} is surface area per reverse micelle. The values of s_{agg} were calculated from the cylindrical core
 515 length and radius ($L_{f\text{-cyl}}$ and $R_{f\text{-cyl}}$) fitted to the SANS data, and assuming 7.4 Å for the surfactant tail length
 516 l_{tail} [16-20]. The calculated EPP values are listed in **Table 1** and plotted as a function of W_0 at different
 517 surfactant concentrations in **Figure 5** (or **Figure S26**).

518

519



520

521 **Figure 5.** Changes in effective packing parameter EPP for reverse micelles as a function of W_0 for
 522 D_2O/CO_2 μ Es with hybrid and double-tail surfactants or D_2O/n -heptane μ Es stabilized by normal AOT
 523 [3,20,26-29,38,39,53]. Experimental conditions were 45 °C and 350 bar for 17mM FC6-HC n ($n = 4-6$)
 524 and 17mM n FG(EO) $_2$ ($n = 4, 8$), 23-40 °C and 380-400 bar for 78 mM Li-F7H4 and 73 mM K-F7H4, 75-
 525 79 mM Na-F7H4, 25 °C and 350-400 bar for 25 mM Ni(di-HCF4) $_2$, 45 °C or 75 °C and 350 bar for 40
 526 mM M(di-HCF6) $_2$ (M=Co and Ni) in D_2O/CO_2 μ Es, 75 °C and 350 bar for 80 mM Na(di-HCF6) in
 527 H_2O/CO_2 μ Es, and 25 °C and 1 bar for 50 mM AOT in D_2O/n -heptane μ Es. The broken circles indicate
 528 formation of rod-like reverse micelles with aspect ratios ($=L_{f-cyl}/(2R_{cyl})$) > 2.5 for each counterion.

529

530 Similar to earlier reports [3,20,26-29,38,39,54], EPP values for the di-HCF6 series decreased
531 with increasing W_0 , consistent with decreases in negative curvature of reverse micelles.

532 Comparing EPP values for all these surfactants, rates of decrease in EPP vs W_0 tend to be steeper
533 with increasing surfactant-ion concentration from 17 mM to 80 mM. On the other hand, divalent
534 counterions Ni^{2+} and Co^{2+} gave rise to lower EPP values compared with monovalent ions Li^+ , Na^+ , and
535 K^+ at the same W_0 values. Comparing Co^{2+} with Ni^{2+} the EPP values for Co^{2+} are smaller, which would
536 fit with the explanation given above for changes in $A_{C/W}$, based on the strength of interactions between
537 $-\text{SO}_3^-$ headgroups and the two different counterions.

538 The broken circles in **Figure 5** indicate formation of rod-like reverse micelles with aspect ratios
539 > 2.5 . From the locations of the broken circles, rod-like reverse micelles appear at $W_0 = 5-20$
540 corresponding to EPP values in the range 1.1-1.8. **Figure 5** also shows that surfactant-ion concentration
541 also plays an important role in generating elongated reverse micelles: the higher the surfactant-ion
542 concentration, the higher the tendency to form rod-like reverse micelles. It is probably due to shortening
543 of the intermicellar distance, which in turn increases the strength of the intermicellar interactions. From
544 these results and discussion, under appropriate EPP, surfactant concentration and W_0 conditions, as well
545 as employing divalent Co^{2+} or Ni^{2+} counterions rod-like reverse micelles can be generated in W/CO_2
546 systems.

547

548 4. Conclusions

549 Dense CO₂ fluids containing reverse micelles with aqueous cores represent interest in, and
550 potentially useful, media for applications such as extraction, dyeing, dry cleaning, enzymatic reaction,
551 and organic/inorganic or nanomaterial synthesis [5]. Regarding enhanced oil recovery using CO₂-flooding,
552 rod-like or worm-like reverse micelles are able to significantly thicken CO₂, improving the currently poor
553 sweep efficiency by preventing fingering phenomenon in reservoirs [2,3]. Previous studies [29] found the
554 hybrid surfactant FC6-HC5 to form rod-like reverse micelles with a length of ~880 Å in W/supercritical
555 CO₂ mixtures at 350 bar and 45 °C. It was estimated that these long and thin micelles would lead to a
556 factor of three increase in CO₂ viscosity: compared to earlier surfactant/W/CO₂ systems [3-13,16-29,34-
557 39] that represents the largest viscosity enhancement of CO₂. Unfortunately, owing to cost and
558 bioaccumulation, these hybrid H-F surfactants are less appropriate for practical applications. On the other
559 hand, it has been shown that low F-content double tail ω-hydroperfluorocarbon anionic surfactants with
560 various counterions Na(di-HCF4), Co(di-HCF4)₂ and Ni(di-HCF4)₂, generate rod-like reverse micelles
561 with lengths of 200-700 Å in liquid CO₂ at 25 °C [38,39]. Although this is very promising for practical
562 uses in EOR, further investigations at higher temperatures, close to reservoir conditions of ~100 °C were
563 needed.

564 This new study investigated the formation of rod-like reverse micelles in supercritical CO₂ under
565 high temperature (75 °C) and pressure 350 bar conditions. The series of surfactants studied here are AOT-
566 like anionic surfactants with different counterions (Na⁺, Co²⁺, and Ni²⁺) and a double CO₂-philic tail with
567 low F-content (di-CF2 series) or ω-hydroperfluorocarbon-type (di-HCF4 and di-HCF6 series), which are
568 more inexpensive, biocompatible and environmentally-benign. Phase behavior observations, viscosity
569 measurements and SANS experiments at [surfactant]/[CO₂] = 0.96 × 10⁻³, 1.92 × 10⁻³, or 3.84 × 10⁻³
570 revealed new findings (1)-(5) as shown below,

571

572 (1) Cylindrical micelles formed by double ω-hydroperfluorohexyl(C₆)-tail surfactants Ni(di-HCF6)₂ and
573 Co(di-HCF6)₂ were able to enhance CO₂ viscosity by factors of 1.94-2.24. This viscosity enhancement

574 is larger than with shorter chain for CF₄-tails and/or the monovalent counterion Na⁺ (**Figures 2 and**
575 **3**). At a water loading of $W_0=10$ the Ni²⁺ counterion surfactant led to higher viscosity than for Co²⁺.
576 In addition, the surfactants with longer ω -hydroperfluorocarbon-tails gave a higher of stability for
577 W/CO₂ mixtures, and at lower CO₂ pressures/densities (**Figure 1**). These results suggest that ω -
578 hydroperfluorocarbon-tails of $> C_4$ and divalent counterions important molecular features for CO₂-
579 thickening surfactants.

580 (2) For most surfactant systems studied here, the relative viscosity η_{rel} was seen to have a maximum at
581 $W_0 = \sim 10$ (**Figure 3**).

582 (3) In these W/CO₂ mixtures the reverse micelle morphology for Ni(di-HCF₆)₂ and Co(di-HCF₆)₂
583 surfactants changed from short rods at $W_0=5 \rightarrow$ long rods (rod length = ~ 260 Å) at $W_0=10 \rightarrow$ short
584 rods or prorates at $W_0=15 \rightarrow$ spheres or oblates at $W_0=20$ (**Table 1**).

585 (4) Following on from (3), the aggregation number N_{agg} M(di-HCF₆)₂ increased with increasing W_0 from
586 5 to 10 commensurate with the formation of long rod-like micelles, but decreased at $W_0 \geq 15$ owing
587 to the formation of two-phase Winsor II systems (**Figures S22 and S23**).

588 (5) Rod-like reverse micelles with aspect ratios > 2.5 appeared at $W_0 = 5-20$ corresponding to effective
589 surfactant packing parameters (EPP) = 1.1-1.8 (**Figure 5**).

590

591 Long rod-like reverse micelles are much more difficult to obtain in W/CO₂ systems than in W/O
592 systems, and are only found with a few specialized FC-surfactants at low temperatures below 45 °C [3-
593 13,16-29,34-39]. As mentioned above, this study demonstrated successful formation of rod-like reverse
594 micelles at a high temperature of 75 °C close to reservoir conditions, and presented molecular design
595 criteria for generating these. The surfactants studied here represent the most successful cases of low F-
596 content additives and hence may make further impacts in this field. As such, long rod-like reverse
597 micelles could offer a new generation of universal solvents with unique properties. Hopefully, the findings
598 described here will be beneficial in the advancement of rod-like reverse micelle systems for CO₂-EOR
599 and nanomaterial synthesis as well as in numerous other applications.

600

601

602 **CRedit authorship contribution statement**

603 M. Sagisaka : Supervision, Writing - original draft, review & editing, Y. Sato : Investigation, S. Kiani :
604 Investigation, S. Alexander : Investigation, T. Ardyani: Investigation, A. Mohamed: Investigation, R. M.
605 Enick : Methodology, S. E. Rogers : Investigation, C. Hill : Investigation, Writing - review & editing, J.
606 Eastoe : Writing - review & editing,

607

608 **Declaration of Competing Interest**

609 There are no conflicts of interest to declare.

610

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619

620 **Appendix A. Supplementary data**

621 Supplementary data associated with this article can be found, in the online version at.

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