



## Review

Nitrogen enriched biochar used as CO<sub>2</sub> adsorbents: a brief review

Yuanting Qiao, Chunfei Wu\*

*School of Chemistry and Chemical Engineering, Queens University Belfast, Belfast, UK BT7 1NN*

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## ABSTRACT

It is widely acknowledged that the increasing CO<sub>2</sub> concentration has led to the rise of temperature in the earth. Thus, capturing CO<sub>2</sub> to alleviate environmental catastrophic is becoming important and urgent. Among the CO<sub>2</sub> sorbents reported, solid adsorbents are advantageous in CO<sub>2</sub> adsorption, CO<sub>2</sub>/N<sub>2</sub> selectivity, easy operation and good regeneration ability. Biochar-based sorbents are promising for CO<sub>2</sub> capture because they are self-sufficient in energy requirements, wide availability, renewability, low cost, and high porous structure. In addition, N-containing functional groups are used to improve the capability of CO<sub>2</sub> adsorption of biochar. This review aims to evaluate the preparation and performance of nitrogen-enriched biochar for CO<sub>2</sub> capture. Throughout this review paper, the current N-containing precursors and biomass, as well as the technologies for the preparation of N-rich biochar are discussed. It is concluded that cheaper and more sustainable ways should be proceeded to produce N-rich biochar in the field of CO<sub>2</sub> capture research.

## 1. Introduction

The atmospheric content of CO<sub>2</sub> concentration has been more than 400 ppm, and CO<sub>2</sub> is a dominant (accounting for 90%) global anthropogenic greenhouse gas ([CO<sub>2</sub> Emissions from Fuel Combustion 2017 Highlights 2017](#)). Fossil fuel combustion, the main energy source, occupies the largest share of the annual CO<sub>2</sub> emissions with over 33 GtCO<sub>2</sub> in 2015 ([Dlugokencky, 2017](#)). To prevent the increase in global temperature, it is essential to control the annual CO<sub>2</sub> emissions ([Siegelman et al., 2017](#)). Therefore, many technologies have been researched to remove CO<sub>2</sub> from ambient air, industry plants, animals and human beings' activities ([Li et al., 2013](#)). Among the variety of routes designed for CO<sub>2</sub> capture from various CO<sub>2</sub> sources, adsorption is regarded as a promising technology ([Samanta et al., 2012](#)). According to the nature of interactions between the adsorbents and CO<sub>2</sub>, adsorption can be classified into physical adsorption and chemical adsorption ([Younas et al., 2016](#)). A variety of porous solids such as zeolites ([Walton et al., 2006](#), [Siriwardane et al., 2005](#)), mesoporous silica ([Harlick and Sayari, 2006](#), [Knowles et al., 2005](#)), metal organic frameworks (MOFs) ([Llewellyn et al., 2008](#), [Millward and Yaghi, 2005](#), [Keskin et al., 2010](#)), porous carbons ([Sevilla and Fuertes, 2011](#), [Sevilla et al., 2011](#)) and porous organics ([de Jonge and Mittelmeijer-Hazeleger, 1996](#)) have been studied for CO<sub>2</sub> removal. In contrast to absorption processes based on a liquid absorbent like monoethanolamine (MEA) ([Abu-Zahra et al., 2007](#), [Glasscock et al., 1991](#)), diethanolamine (DEA) ([Glasscock et al., 1991](#), [Haji-Sulaiman et al., 1998](#)) and potassium carbonate ([Cullinane and Rochelle, 2004](#)), a solid adsorbent is used to bind the CO<sub>2</sub> on its sur-

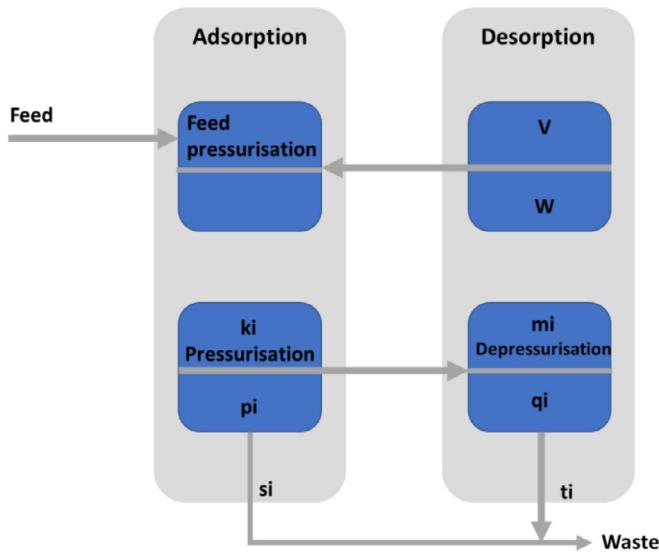
faces with many advantages including greater capacity, high selectivity, flexible handling and easy regeneration ([Samanta et al., 2012](#), [Qi et al., 2011](#)). The regeneration of adsorbents depends on Temperature swing adsorption (TSA), pressure swing adsorption (PSA), and vacuum swing adsorption (VSA). PSA systems have been applied in industrial feed mixtures such as steam reformer off the gas, landfill gas, and natural gas, where the feed gas at high pressure and low temperature offers the driving force between the desorption pressure and the adsorption pressure. Chung et al. ([Ho et al., 2008](#)) illustrated the PSA using the "short-cut" method that PSA systems rely on batch sorption vessels with a fixed volume, as shown in [Figure 1](#).

Activated carbon is one of the most solid adsorbents that are applied in the PSA unit ([Shen et al., 2015](#)). The preparation of activated carbon normally contains heat treatment of carbon materials such as biomass, coal, oil and peat, as well as activation steps including both chemical and physical activation ([Ioannidou and Zabaniotou, 2007](#)). The chemical activation relied on the chemical activating agent such as KOH, NaOH, H<sub>3</sub>PO<sub>4</sub>, K<sub>2</sub>CO<sub>3</sub>, ZnCl, etc, which are usually expensive and bad for the environment ([Shafeeyan et al., 2010](#)). In terms of industrial application, activated carbons are commonly produced from biomass via KOH activation. Thus, single-step preparation or only activation of biomass with steam without extra carbonisation or pyrolysis step is more appealing, which has also been shown to produce good quality adsorbents ([Zhang, 2015](#)).

Biochar is a solid carbon material, which has been successfully applied to improve soil quality ([Sohi et al., 2010](#), [Lehmann et al., 2011](#)), remove contaminants in water and soil ([Ahmad et al., 2014](#)), reduce greenhouse gas emissions ([Bamdad et al., 2018](#), [Jung et al., 2018](#)).

\* Corresponding authors. Dr Chunfei Wu, Tel: +44 2890975573.

E-mail address: [c.wu@qub.ac.uk](mailto:c.wu@qub.ac.uk) (C. Wu).



**Figure 1.** Short-cut method of VSA/PSA process (Ho et al., 2008). The processes of pressurization and adsorption and the processes of depressurization and desorption are combined.  $\text{CO}_2$  is adsorbed at higher pressure and desorbed at lower pressure, under adiabatic conditions. The adsorption and desorption can be modeled by the Langmuir isotherm.  $K_i/m_i$ , amount of component  $i$  in the bulk gas;  $s_i/t_i$  amount of component  $i$  in the expelled gas;  $p_i/q_i$ , amount of component  $i$  on the adsorbent.  $W$ , the weight of the adsorbent;  $V$ , the volume of the adsorbent.

2019, Mohd et al., 2013), and reduce energy production (Zhang et al., 2019, Lehmann et al., 2006), etc. (Ahmed et al., 2016, Keiluweit et al., 2010, Rittl et al., 2018). Currently, biochar is also acknowledged as an eco-friendly and cheap  $\text{CO}_2$  adsorbent, which is nearly ten times cheaper than others such as MOFs and commercial activated carbon (Mohd et al., 2013, Pashetti et al., 2015, Dissanayake et al., 2020) due to the cheap and environmental-friendly source of biomass materials such as bamboo (Wei et al., 2012), fungi (Wang et al., 2012), yeast (Shen et al., 2012), chitosan (Wang et al., 2020), nutshell (Deng et al., 2014), palm shells (Ello et al., 2013), coconut shell (Yang et al., 2011), coffee ground (Plaza et al., 2012), cassava peel (Moreno-Piraján and Giraldo, 2010), celtuce leave (Wang et al., 2012), potato starch and cellulose (Sevilla and Fuertes, 2011), of which are most waste. Moreover, biochar is usually prepared by pyrolysis at moderate temperatures (usually below 700 °C) in an oxygen-deficient or oxygen-free environment (Balahmar et al., 2017). The pyrolysis process is attractive as it has the following advantages: (1) Biochar can usually satisfy energy requirements with extra energy production in the form of heat or biofuel (Matovic, 2011). (2) Biomass is renewable, the most abundant, worldwide available, inexpensive and environmentally friendly; thus, biochar is cheap and environmental friendly (Ioannidou and Zabaniotou, 2007, Plaza et al., 2014). (3) Biochar shows well in high surface area, which is beneficial for  $\text{CO}_2$  capture (Ok et al., 2015).

Generally, the  $\text{CO}_2$  adsorption of biochar depends on both physical and chemical properties such as the porosity, basicity of biochar surface, surface functional groups, presence of alkali and alkali earth metals, hydrophobicity, polarity, and aromaticity (Chiang and Juang, 2017). These properties are influenced by the route of preparation, carbon source, activation, and modification such as chemical modification, physical modification, impregnation with elements, or grafting, as well as pretreatment/post-treatment of the feedstock (Igalavithana et al., 2017). Nitrogen has been reported to enhance the good adsorption and selectivity of porous carbon (Ahmed et al., 2016) because N-rich functional groups can enhance the surface affinity between basic sites and  $\text{CO}_2$ , as well as microporous structure, large pore volume and surface area in some cases (Z-L et al., 2013, Ma et al., 2013). For

example, amazonian wastes (nutshells waste) improved by nitrogen flow, have been reported to produce N-rich porous carbon used for  $\text{CO}_2$  adsorbents (Serafin et al., 2021). The highest capacity of  $\text{CO}_2$  adsorption reached at 298 K with 3.67 mmol g<sup>-1</sup>. A pinewood derived biochar was investigated with amine activation (tetraethylenepentamine, TEPA) and showed the capacity of  $\text{CO}_2$  capture up to 2.79 mmol g<sup>-1</sup> (Chatterjee et al., 2018).

To date, several reviews have discussed the modification with nitrogen groups to enhance the  $\text{CO}_2$  capture of activated-carbon-based adsorbents (Shafeeyan et al., 2010, Saha and Kienbaum, 2019). The main objective of this paper is to analyse the modification of biochar with N-containing groups and the possible N-rich biomass sources to produce biochar, as well as the performance and the mechanism of the N-rich biochar used as  $\text{CO}_2$  adsorbents.

## 2. Nitrogen source for the N-rich biochar

N-functional groups introduced into biochar have been applied in many fields such as adsorbents for heavy metal (Jia et al., 2002) and  $\text{SO}_2$  (Shao et al., 2018), catalysis (Guo et al., 2016), energy storage (Yaumi et al., 2017), etc (Leng et al., 2020). There are two main sources of nitrogen. One is introducing the nitrogen-containing functionalities to modify the biochar; the other is the direct use of the nitrogen-rich biomass.

### 2.1. N-containing functionalities

Usually, ammonia, amine groups (including primary amine, secondary amine and tertiary amine), and polymer-based amine are used to introduce N into biochar. Amine groups strongly and selectively bind  $\text{CO}_2$  via chemisorptive interactions with  $\text{CO}_2$  molecules by forming a carbamate (Xiong et al., 2013). Ammonia is widely used as the N functionalities. Zhang et al. used black locust to produce ammonia-doped biochar, AC-KOH-N, with activation of KOH and ammonia ( $\text{NH}_3$ ) under  $\text{N}_2$ , at 830°C (Zhang et al., 2016). At 1 bar,  $\text{CO}_2$  adsorption reached 5.05 mmol g<sup>-1</sup> at 25 °C and 3.37 mmol g<sup>-1</sup> at 50 °C.  $\text{CO}_2/\text{N}_2$  selectivity of AC-KOH-N calculated by the IAST method was 30.75 at 25 °C and 1 bar, and  $\text{CO}_2$  adsorption of AC-KOH-N was fully reversible and stable after 10 cycles.

As urea is a cheap and non-toxic amine group, it is also commonly used to introduce nitrogen into porous material. Cansado et al. has compared activated carbon with the treatment of sodium hydroxide and urea, and the results showed that the urea treatment could lead to better porosity and a basic character; whereas, the treatment with sodium hydroxide showed little influence on the nature of activated carbon (Cansado et al., 2012). Rouzitalab et al. used walnut shell, activated by urea and following KOH, to produce biochar, which shows  $\text{CO}_2$  adsorption capacity of 7.42 mmol g<sup>-1</sup>, and  $\text{CO}_2/\text{N}_2$  selectivity of 12.7 at 25 °C and 1 bar (Rouzitalab et al., 2018).

Melamine has also been used as a nitrogen source to modify a wafer chestnut for the prepare N-rich biochar through KOH activation at 600 °C-900 °C (Wei et al., 2018). The resulting samples showed highly developed micropores, outstanding surface area (3401 m<sup>2</sup> g<sup>-1</sup>) and a high nitrogen content (4.89 at.%), leading to  $\text{CO}_2$  adsorption capacity up to 6.0 mmol g<sup>-1</sup> at 0 °C and 1 bar and 4.7 mmol g<sup>-1</sup> at 25 °C and 1 bar.

### 2.2. N-rich biomass

Compared to the N-containing functionalities, biomass derivatives as precursors are more sustainable and available (Zhao et al., 2010). Some biomass samples that have a high content of nitrogen have been concluded in Table 1 (Leng et al., 2020). Microalgae occupies the highest N-content with 13.94%, and its turning biochar is 6.57%–12.93%. Chitosan also performs well with the 9.4% N-content in biomass and 8.9–9.1% N-content in produced biochar. In addition, the porous carbon

**Table 1**

Nitrogen content and form of nitrogen in biomass and derived porous carbon (Leng et al., 2020).

Biomass Biomass	N(w%)	Form	Porous carbon N(w%)	Form	Application	Ref.
Sludge	5.9	Protein-N	2.1–3.1	Pyridinic-N	Adsorbents for ammonium in water	(Tang et al., 2019)
Sewage sludge	6.2	-	2.1–7.1	-	Adsorbents for heavy metal	(Agrafioti et al., 2013)
Wood sawdust	0.41	-	0.56–0.71	-	Catalyst for esterification and transesterification	(Chellappan et al., 2018)
Organic xerogel	0.41	-	0.28–5.84	-	Adsorbents for heavy metal	(Veselá and Slovák, 2014)
	0.53		0.15–5.7			
Alfalfa	2.4	-	4.0–4.9	-	Adsorbents for bisphenol A and sulfamethoxazole in water	(Choi and Kan, 2019)
Rice Husk	1.20	-	0.41–1.23	-	Renewable solid bio-fuel source	(Abbas et al., 2018)
Rice Husk	-	-	0.01–1.05	-	Galaxolide adsorbents	(Zhang et al., 2019)
Wheat straw	-	-	0.01–0.52	-	Galaxolide adsorbents	(Zhang et al., 2019)
$\alpha$ -amylase	-	-	1.39–8.60	C–N	Adsorbents for aromatic compounds	(Zhang et al., 2014)
Chitin	-	-	2.86–10.13	-		
Zein	-	-	2.50–14.92	-		
Microalgae	13.94	Pyrolic-N, pyridinic-N	6.57–12.93	C–N–C, pyrolic-N, pyridinic-N, quaternary-N	Nitrogen-containing compounds such as indole, quinoline, isoquinoline and phenanthridine	(Maliutina et al., 2018)
Gelatin	-	-	9.26–0.88	Pyridinic, pyrolic/pyridone, quaternary, and pyridine-N-oxide	Supercapacitors	(Xu et al., 2012)
Pine-cone	-	-	1.9–2.0	-	Rremoving tetracycline	(Wu et al., 2021)
Chitosan	9.4	-	8.9–9.1	-		(Zhao et al., 2010)
Glucosamine	6.5	-	6.6–6.7	Pyridinic and aromatic graphene structure	-	(Zhao et al., 2010)
Cotton stalk	1.09	–NH, –NH <sub>2</sub> , protein-N	0.47–1.28	N–H, N–COO, C–N, C = N, pyridinic-N	CO <sub>2</sub> adsorbents	(Zhang et al., 2014)
Cotton stalk	1.15	protein-N	1.02–1.09	N–H, C–N, C = N, amine-N, pyridinic-N	CO <sub>2</sub> adsorbents	(Xiong et al., 2013)
Walnut shell	4.5	-	0.34–1.54	-	CO <sub>2</sub> adsorbents	(Lahijani et al., 2018)
Rice Husk	0.38	-	0.33–0.52	C–N, N = O, pyridinic-N	CO <sub>2</sub> adsorbents	(Zhang et al., 2015)
London plane leaves	0.2	-	0.4–2.5	Pyridinic and pyridonic	CO <sub>2</sub> adsorbents	(Zhu et al., 2015)
Pine-cone	0	-	0.5–1.3	Pyrolic	CO <sub>2</sub> adsorbents	(Zhu et al., 2016)
Soybean straw	1.52	-	1.34–1.46	-	CO <sub>2</sub> adsorbents	(Zhang et al., 2016)
Digestate from Anaerobic Digestion	1.82	-	1.88–2.30	-	CO <sub>2</sub> adsorbents	(Qiao et al., 2020)

derived from Zein reaches up to 14.92%. Most nitrogenous groups in the biomass exist in the form of both inorganic N-functional groups (e.g. NH<sub>4</sub>–N, NO<sub>2</sub>–N, and NO<sub>3</sub>–N) (Liu et al., 2018) and organic N-functional groups (e.g. pyridinic-N, pyrolic-N, quaternary-N, pyridinic-N-oxide, graphitic-N, amine-N, amide-N, nitrile-N, etc.) (Yuan et al., 2018). After pyrolysis, nitrogen-rich components may convert into pyridinic-N, pyrolic-N, quaternary-N, and possibly pyridinic-N-oxide (Chen et al., 2017). Generally, the higher nitrogen content leads to the higher nitrogen content of porous carbon. However, the pyrolysis may also lead to the loss of nitrogen in the biomass as the nitrogen-containing groups may convert into nitrogen-containing gases (e.g. NH<sub>3</sub>). Among the nitrogen-containing biomass including cotton stalk, walnut shell, rice husk and london plane leaves have been used to produce biochar as CO<sub>2</sub> adsorbents. However, these biomass are not outstanding nitrogen content of biomass, more possibilities can be further explored.

### 3. Preparation of N-rich biochar

Biochar is mainly activated carbon through physical and chemical methods. In chemical activation, the precursor is carbonised using chemical agents such as KOH, NaOH, H<sub>3</sub>PO<sub>4</sub>, K<sub>2</sub>CO<sub>3</sub>, ZnCl, etc. In terms of industrial application, activated carbons are commonly produced from biomass via KOH activation. However, the chemical activation via washing procedures eliminates the excess activating agent from the biochar. In contrast, physical activation is benign to the environment with activating agents such as CO<sub>2</sub>, H<sub>2</sub>O or air as. The disadvantages of the activation technologies relate to the remarkable loss of mass, nitrogen, and other heteroatoms. Generally, N-rich porous carbons have been prepared through some methods: (1) In-situ pyrolysis of N-containing functional groups or N-rich biomass. (2) Post-modification with N-containing functional groups.

### 3.1. In-situ pyrolysis

In-situ pyrolysis of N-containing functional groups and biomass are the most promising way to prepare N-rich biochar. It is required to mix the N-containing functional groups and biomass before pyrolysis through the methods such as the impregnation method, gaseous activation, mixing, etc. Impregnation is normally used to chemically modify the adsorbents. For example, the amine is typically dissolved in a polar solvent such as methanol or ethanol and subsequently mixed with the porous carbon (Chen et al., 2014). Madzaki et al. compared biochar from raw sawdust without the modification to the amine-modified biochar through the amine impregnation with monoethanolamine (MEAs) (Madzaki and KarimGhani, 2016). It was shown that the impregnation reduced the BET surface area of biochar attributed to the pore filling effects of the nitrogen. In addition, the impregnation method did not enhance basic functionalities linked to the surface of the biochar. Thus, the modified biochar showed less CO<sub>2</sub> adsorption compared to the biochar without modification, although it had a higher N-content but lower BET surface area.

To overcome these disadvantages, ammonia treatment was explored to introduce the N-functionalities to porous carbon. Generally, gaseous activation was proved to increase porosity between 700 and 800°C, which can be attributed to high reaction rates of steam with carbon (Gergova and Eser, 1996). In addition, ammonia is used as a modification method. For example, Zhang et al. reported a cotton stalk-derived biochar prepared by pyrolysis and modification by gaseous NH<sub>3</sub> (Zhang et al., 2014). The surface area of CA-char was the highest at 627.15 m<sup>2</sup> g<sup>-1</sup>, and its CO<sub>2</sub> adsorption capacity was 2.18 mmol g<sup>-1</sup> at 20°C when N content was 1.52%. Using the method, CN 800 was obtained from soybean straw by modification of CO<sub>2</sub>-NH<sub>3</sub> mixture at 800°C, processing CO<sub>2</sub> adsorption of 88.89 mg g<sup>-1</sup> (Zhang et al., 2016).

Another challenge that lies in the activation technologies is the significant mass loss during activation. Mixing between solids is also one efficient way to introduce the nitrogen groups to avoid mass loss. Our group has also proposed a one-step method to obtain N-rich biochar derived from anaerobic digestion digestate used as a CO<sub>2</sub> adsorbent (Qiao et al., 2020). The N-rich biochar was obtained by pyrolysis of a mixture of the biomass and urea, with the CO<sub>2</sub> capacity up to 1.22 mmol g<sup>-1</sup>. In this work, the low BET surface area limited the CO<sub>2</sub> capacity, which may be linked to blocked pores. However, both the porous property and functionalities are important to CO<sub>2</sub> capture.

Peiyu et al. used a “mixed molten salt” method to receive hierarchical N-rich activated carbons (N-ACs) derived from chitosan with a molten salt template of LiCl-ZnCl<sub>2</sub> (Wang et al., 2020). This simple one-step carbonization method is also advantageous in terms of avoiding significant mass loss. The CO<sub>2</sub> adsorption capacity of N-ACs was 7.9/5.6 mmol•g<sup>-1</sup> at 0°C/25°C under 1 bar pressure, respectively.

Generally, the process of biochar production used for CO<sub>2</sub> capture is conducted by two steps including carbonization and activation, which means harsh and multiple processes are used. But if the biochar is prepared through a single-step process, its costs could be decreased.

### 3.2. Post modification

Biochar from coffee grounds was reported to be treated by three methods as follows: (i) KSHC, dispersion of the biochar in an alcohol solution of 3-aminopropyltrimethoxysilane (APTES), (ii) KPHC, through the polycondensation of C<sub>6</sub>H<sub>5</sub>NH<sub>2</sub>, and (iii) KMHC, hydrothermal treatment with melamine solution of biochar at 160 °C for 24 h (Liu and Huang, 2018). KMHC led to the highest CO<sub>2</sub> adsorption (117.51 mg/g) among three prepared adsorbents, possibly due to the presence of high microporosity, good N content (5.1 wt%) with active sites (pyrrolic nitrogen). These sorbents also showed surpassing renewability and cyclability.

Nguyen et al. prepared a biochar (AMBC, porous nitrogen-doped biochar) sorbent at lower pyrolysis and modification temperature with

higher CO<sub>2</sub> adsorption (Nguyen and Lee, 2016). The preparation method was also based on the gas modification but a little complex, with the following steps: (1) slow pyrolysis of chicken manure for 1 h at 450°C; (2) chemical treatment from HNO<sub>3</sub> and anhydrous ammonia gas for 1 h at 450°C; (3) reaction with sodium-*l*-gulopyranuronate to form solid beads. The AMBC beads performed a high capacity of CO<sub>2</sub> adsorption (10.15 mmol g<sup>-1</sup> at 20°C) with a specific surface area (328.6 m<sup>2</sup> g<sup>-1</sup>) and CO<sub>2</sub>/N<sub>2</sub> selectivity (79.1). Another important performance was the stability in that the CO<sub>2</sub> adsorption capacity kept 85% after ten regeneration cycles.

To simplify the preparation procedure, Serafin et al. used a one-step method of combining carbonization with activation to make use of Amazonian wastes (nutshells waste), including Andiroba (AD), Biochar Brazilian nut (BBN), Brazilian nutshell (BNS), Cascara Cupuassu (Cas-Cup), COSC Cupuago (CosCup), Hueso Assai (HA), to produce biochar-based CO<sub>2</sub> adsorbents (Serafin et al., 2021). The highest capacity of CO<sub>2</sub> adsorption at 298 K with 3.67 mmol g<sup>-1</sup> was investigated on Cascara Capuassau-derived biochar.

Riya et al. described pinewood-derived biochar via a two-stage activation process including sonication treatment and amine-activation (tetraethylenepentamine,TEPA) near room temperature (Chatterjee et al., 2018). The optimum capacity of CO<sub>2</sub> capture was 2.79 mmol g<sup>-1</sup> at 70 °C, 0.15 atm. The method of post-modification is related to high consumption of energy or cost because of high temperatures, corrosive materials, blocked pores.

From table 2, the highest capacity of CO<sub>2</sub> capture is 10.15 mmol/g at 20°C for AMBC. Because of the existence of CO<sub>2</sub> and N<sub>2</sub> in flue gas from fossil-fuel power plants, CO<sub>2</sub>/N<sub>2</sub> selectivity is a key factor for the development of biochar-based adsorbents. The highest CO<sub>2</sub>/N<sub>2</sub> selectivity is also obtained using AMBC, with 79 at 20°C. However, the highest BET surface area is KNWS-xy with 4230 m<sup>2</sup> g<sup>-1</sup> and the highest N-content with 8.99% is from UCAD 1:1. Researchers have discussed the co-effect of BET surface area, N-functionalities on the CO<sub>2</sub> adsorption (Wei et al., 2012, Gupta and Kua, 2017). During the preparation of AMBC, the chemical treatment of the biochar with HNO<sub>3</sub> and NH<sub>3</sub> enhanced the presence of amine groups on its surface, thus leading to the increased capacity of CO<sub>2</sub> capture. Therefore, it is desirable to directly convert biomass into porous carbon with good CO<sub>2</sub> capacities. In addition, the comparison between the sample before and after nitrogen enrichment proves that N-functionalities have a larger contribution to CO<sub>2</sub> adsorption compared to BET surface area. In all the cases shown in table 2, CO<sub>2</sub> adsorption has been improved after nitrogen is enriched, while in some cases like USO.5-EH 1:1-T2.5 (Chatterjee et al., 2018), BET surface area decreased after the introduction of nitrogen.

In terms of preparation methods, the post-modification method requires more steps and the possibility of pore blockage. Thus the in-situ method is a preferred method (Rouzitalab et al., 2018).

### 4. Mechanism of CO<sub>2</sub> adsorption on N modified biochar

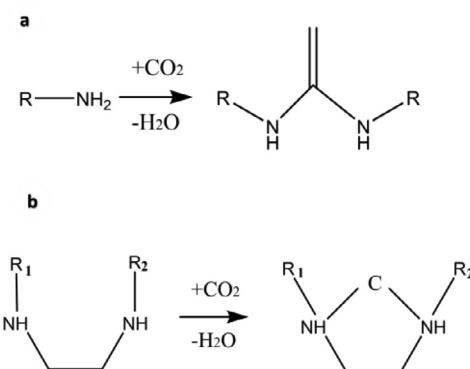
Nitrogen atoms can replace carbon atoms in carbon materials as nitrogen atoms are close to C atoms in the periodic table. The covalent radius of carbon is 0.77 Å, while the nitrogen is 0.74 Å (Lv et al., 2018).

When the heteroatomic nitrogen is introduced into a porous carbon, the surface conjugate structure and electron distribution of the carbon carrier, as well as the electrical neutrality of carbon materials, are changed (Wu et al., 2019). N-containing groups were reported to perform well in CO<sub>2</sub> adsorption, CO<sub>2</sub>/N<sub>2</sub> selectivity, and initial isosteric heats of CO<sub>2</sub> adsorption (Qst) with improved surface properties (Wickramaratne et al., 2014).

The nitrogen in porous carbon mainly contributes to the chemical adsorption of CO<sub>2</sub> instead of the physical adsorption of CO<sub>2</sub> (Chen et al., 2013). Primary and secondary amines formed various urea linkages in the reactions between the N-containing groups and CO<sub>2</sub> (Sayari et al., 2012, Sethia and Sayari, 2014). As shown in Fig. 2, primary amines form open-chain urea with CO<sub>2</sub> (Route a, Fig. 2), which is regarded as

**Table 2**  
Summary for representative reported CO<sub>2</sub> adsorbents of N-rich biochar at 1 bar.

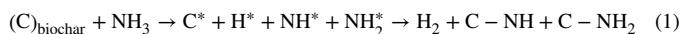
Sample Name	Before Nitrogen enrichment			After Nitrogen enrichment			Ref.
	Biomass	BET Surface area/ m <sup>2</sup> g <sup>-1</sup>	CO <sub>2</sub> adsorption/mmol g <sup>-1</sup>	BET Surface area/ m <sup>2</sup> g <sup>-1</sup>	CO <sub>2</sub> adsorption/mmol g <sup>-1</sup>	CO <sub>2</sub> /N <sub>2</sub> selectivity	
N-AC-3-1000	Chitosan	-	-	2025	5.6 at 25°C	-	(Wang et al., 2020)
CasCup	Nutshell waste	-	-	1624	5.13 at 0°C 3.67 at 20°C, 48 at 20°C	(Serafin et al., 2021)	
USO.5-EH 1:1-T2.5	Pinewood	312.31	0.3 at 70 °C	261.68	2.79 mmol/g at 70 °C and 0.15 atm	-	(Chatterjee et al., 2018)
AC-KOH-N KNWS-xy	Black locust Walnut shell	1175 2.19	1.85 at 25°C -	2511 4230	5.05 at 25°C 7.42 at 25°C	31 at 25°C 13 at 25°C	(Zhang et al., 2016) (Rouzitalab et al., 2018)
ANCs-3-700	Water chestnut	15	-	3401	4.7 at 25°C	-	(Wei et al., 2018)
A-char	Cotton stalk	224	-	627	2.18 at 20°C	-	(Zhang et al., 2014)
PC3-700	Pine cones	-	-	2090	-	-	(Zhu et al., 2016)
NSD 850	Raw sawdust	-	1.08 at 30°C	3.17	1.02 at 30°C	-	(Madzaki and KarimGhani, 2016)
CN 800	Soybean straw	0.04	0.96 at 30°C	491	2.02 at 30°C	-	(Zhang et al., 2016)
UCAD 1:1	Digestate from Anaerobic Digestion	-	-	6.89	1.22 at 25°C	-	(Qiao et al., 2020)
KSHC	Coffee grounds	34	0.14 at 35°C	1684	2.04 at 35°C	-	(Liu and Huang, 2018)
KPHC				992	2.22 at 35°C	-	
KMHC				990	2.67 at 35°C	74 at 35°C	
AMBC	Chicken manure	34.6	3.72 at 20°C	328.6	10.15 at 20°C	79 at 20°C	(Nguyen and Lee, 2016)
GSK1-700	Starch, Pristine gelatin	1294	3.3 at 25°C	1636	3.84 at 25°C	51 at 25°C	(Alabadi et al., 2015)



**Fig. 2.** The mechanism of reaction between amines and CO<sub>2</sub> (Abbas et al., 2018).

the main reaction. As for adsorbents containing ethylenediamine units, the mechanism will be the reaction between secondary amines and CO<sub>2</sub> to obtain cyclic urea (Route b) (Sayari et al., 2012).

For example, the enhancement of CO<sub>2</sub> adsorption by ammonia treatment depended on the C–N and C=N groups introduced by modifications (Przeplórski et al., 2004). In detail, NH<sub>3</sub> decomposes to produce various free radicals including NH<sub>2</sub><sup>\*</sup>, NH<sup>\*</sup>, and H<sup>\*</sup> when the temperature is around 500 °C. Then these radicals react with the active sites on the surface of biochar to form N-containing functionalities such as amines, amides, imides, lactams, nitriles, or pyridine- or pyrrole-like functional groups as shown in the following routes (Scheme 1) (Li et al., 2019).



## 5. Conclusion

In terms of N sources, N-containing functionalities and N-rich biomass are introduced into biochar to enhance CO<sub>2</sub> adsorption. Ammonia, urea and polymer-based amine have been applied as the functionalities, while microalgae and chitosan are significantly N-rich biochar. The preparation methods include in-situ pyrolysis and post-modification

with N-containing functional groups. The further design may lie in the combination of both the nitrogen-rich functionalities and nitrogen-rich biomass groups together. As most of the methods for preparing biochar based CO<sub>2</sub> adsorbents require at least two steps including pyrolysis and modification. Thus, a simpler process is desired, for example, the one-step in-situ method of combining carbonization with activation to make use of N-compounds in biomass to obtain active biochar for CO<sub>2</sub> capture. Biochar based adsorbents for CO<sub>2</sub> capture have shown high activity, good selectivity, stability after regeneration cycles and nontoxicity to the environment.

## Declaration of Competing Interest

There are no conflicts of interest to declare.

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